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## Optimization of the metakaolin geopolymer preparation for maximized ammonium adsorption capacity

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### Abstract

Geopolymers are functional materials that can be used in various environmental applications such as adsorbents in pollutant removal from wastewaters. Metakaolin geopolymer (MK-GP) has been proven to be especially suitable for ammonium ( $\text{NH}_4^+$ ) removal from wastewater. In this research, the optimal reagent and raw material ratios in the preparation of MK-GP in terms of  $\text{NH}_4^+$  adsorption capacity were investigated. The response surface methodology based on the face centered central composite design was used to optimize the levels of three factors: the amounts of hydroxide, silicate, and metakaolin. In addition, the effect of Na or K as the charge-balancing cation was studied. Empirical models were fitted to the experimental data using multiple linear regression. The significance of the models was confirmed by means of analysis of variance. Optimal  $\text{NH}_4^+$  removal efficiency was achieved when the amount of hydroxide and silicate were maximized, the amount of metakaolin was minimized, and Na-based reagents were used. These trends are most likely a result of optimized conversion of metakaolin into MK-GP.

Keywords: adsorption; ammonium removal; geopolymer; statistical experiment design; wastewater treatment

## 1. Introduction

Geopolymers are defined as materials formed by a reaction between alkali activator (concentrated aqueous solution of e.g. alkali hydroxide and silicate) and solid aluminosilicate precursors (such as metakaolin or fly ash) [1, 2]. However, also materials obtained from a reaction between alumino-silicate precursors and phosphoric acid are sometimes referred to as acid-activated geopolymers [3]. Geopolymers have recently gained interest in several water and wastewater treatment applications such as adsorbents [4-11], membrane material [12], photocatalysts [13, 14], functional construction materials [15, 16], or substrate for biofilm reactors [17]. In many of the aforementioned applications, the use of geopolymers is based on their ion exchange capacity and porous structure.

One interesting use for metakaolin-based geopolymer (MK-GP) is in ammonium ( $\text{NH}_4^+$ ) removal from wastewater [18].  $\text{NH}_4^+$  is the most significant nitrogen species contributing to the eutrophication of water bodies when nitrogen is the nutrient in shortest supply. The main advantage of MK-GP over the conventional biological nitrification-denitrification process is the lower dependency on temperature since it works as a cation exchanger [18]. Furthermore, MK-GP has been shown to be regenerable, more effective than typical natural zeolites, and simpler to produce than synthetic zeolites which require higher synthesis temperature [18, 19].

Although there is already an appreciable amount of papers published on the adsorption properties of geopolymers, only few studies have aimed to systematically determine the impact of preparation conditions on adsorption efficiency. Wang et al. [20] and Li et al. [21] showed that the increased curing temperature and the sodium to fly ash weight ratio up to a certain point improved the  $\text{Cu}^{2+}$  removal efficiency when preparing fly ash-based geopolymers by the fusion method. It is known that the elevated temperature promotes the formation of crystalline zeolitic phases [22] and specific surface area of geopolymers correlates linearly with a geopolymer sample zeolite content [23]. Furthermore, the amounts of  $\text{SiO}_2$ ,  $\text{Al}_2\text{O}_3$ ,  $\text{H}_2\text{O}$ ,  $\text{OH}^-$ , and cations in the reaction mixture affect the structure of geopolymer [24]. However, the relationship between geopolymer preparation parameters and adsorption efficiency is not well understood.

In order to obtain a maximal  $\text{NH}_4^+$  adsorption capacity and to understand the impact of preparation conditions and formulation, the synthesis of MK-GP needs to be optimized. Statistical experimental design is a reliable approach for studying the effects of experimental variables and to optimize their levels in many branches of science [25]. A face centered central composite design (CCF) was used in this study to optimize the preparation conditions of MK-GPs. CCFs provide information on the effects of experimental variables with a minimum number of experiments. A response surface model can be fitted to the experimental data. After validation, the model will show how changes in variable levels affect a response of interest and can be used to find the levels of variables that will optimize the response. A CCF design requires three levels for each factor.

In this research, the influences of the amounts of hydroxide, silicate, and metakaolin used for the preparation of MK-GPs on  $\text{NH}_4^+$  adsorption were investigated. Furthermore, the experiments were conducted with Na and K hydroxide and silicate to observe the effect of the charge-balancing cation. The experiments for the preparation of MK-GPs were carried out according to CCF, the geopolymers were characterized for their physico-chemical structure, and tested for  $\text{NH}_4^+$  removal using model solutions. The experimental design was prepared and the data was analyzed using the MODDE software ([www.umetrics.com](http://www.umetrics.com)).

## 2. Materials and methods

### 2.1 Experimental design

The effects of three factors on the response was investigated and optimized using a CCF design. Factors represent the corresponding amounts of hydroxide, silicate and metakaolin used in the preparation of geopolymer specimen. The levels of the factors (Table 1) were selected according to our previous research [18]. 17 experiments as duplicates (total 34 experiments) were conducted in a random order for both Na and K-based MK-GPs (Table 2). Statistical analysis of the results gained from the batch adsorption experiments were performed with the MODDE 9.1 software. A quadratic model was fitted to the data using multiple linear regression (MLR) and the significance of the model was tested by means of analysis of variance (ANOVA) with a 95% confidence level.

Table 1. The levels of experimental factors in the CCF design.

Factor	Na-based MK-GPs			K-based MK-GPs		
	Low (-1)	Intermediate (0)	High (+1)	Low (-1)	Intermediate (0)	High (+1)
A: Hydroxide [g]	6.24	7.455	8.67	8.29	9.81	11.33
B: Silicate [g]	7.95	8.835	9.72	8.07	8.965	9.86
C: Metakaolin [g]	50	65	80	50	65	80

Table 2. Design matrix for the three-level CCF design.

Exp No	Exp Name	Run Order	Levels of factors <sup>b</sup>		
			A: Hydroxide	B: Silicate	C: Metakaolin
1	MK-M-N1 <sup>a</sup>	7	-1	-1	-1
2	MK-M-N2	5	+1	-1	-1
3	MK-M-N3	16	-1	+1	-1
4	MK-M-N4	14	+1	+1	-1
5	MK-M-N5	4	-1	-1	+1
6	MK-M-N6	17	+1	-1	+1
7	MK-M-N7	11	-1	+1	+1
8	MK-M-N8	8	+1	+1	+1
9	MK-M-N9	15	-1	0	0
10	MK-M-N10	6	+1	0	0
11	MK-M-N11	2	0	-1	0
12	MK-M-N12	9	0	+1	0
13	MK-M-N13	10	0	0	-1
14	MK-M-N14	13	0	0	+1
15	MK-M-N15	12	0	0	0
16	MK-M-N16	3	0	0	0
17	MK-M-N17	1	0	0	0

<sup>a</sup> = M is Na or K, <sup>b</sup> = coded levels, for real levels, see Table 1.

## 2.2. Preparation of metakaolin geopolymers

The reagents used for the preparation of GPs were NaOH (VWR Chemicals, > 97%), Na silicate (VWR Chemicals, SiO<sub>2</sub> 26.8%, Na<sub>2</sub>O 8.2%), KOH (Merck, ≥ 85%), and K silicate (obtained from a Finnish supplier, Sateenkaari Perinnetaito Ltd, SiO<sub>2</sub> 24.5%, K<sub>2</sub>O 11%). Powdered metakaolin was obtained from Aquaminerals Finland Ltd.

The geopolymers were prepared as follows: 8, 10, or 12 M NaOH or KOH solution was mixed with Na or K silicate (0.8:1, 1:1, or 1.2:1 w/w) in order to obtain the levels shown in Table 1. The alkaline solution was allowed to stand for 24 h before use, in order to allow the silicate solution to depolymerize. Metakaolin was then mixed with the alkaline solution in the ratios (w/w) of 1:1, 1.3:1, or 1.6:1 in order to obtain the amounts according to the CCF design (Table 1). The paste was then mixed for five minutes and allowed to consolidate at room temperature for three days. The geopolymer specimens were then crushed and sieved to the particle size of 63–125 µm. Before use, the materials were washed carefully with distilled water, dried at +105 °C and stored in a desiccator.

## 2.3 Characterization of metakaolin geopolymers

The crystalline phases in MK-GPs were characterized with an X-ray diffractometer (PanAnalytical Xpert Pro) using Co K $\alpha$  radiation generated at 40 kV and 40 mA. XRD patterns were collected in the range of 5–80°2 $\theta$  using a scan time of 1.25 s per 0.02°. Samples were prepared by dispensing a finely ground specimen with ethanol onto a glass plate and allowing the ethanol to vaporize before measurement. Diffractograms

were interpreted using the Highscore software (version 3.0) and the Chrystallography Open Database, the 2013 version.

The elemental composition of samples was determined semiquantitatively with an X-ray fluorescence (XRF) spectrometer (PanAnalytical Minipal 4) and the Omnia software. Samples were ground to a fine powder and compressed to tablets before analysis. Loss on ignition (LOI) value was determined using a thermogravimeter (Linseis STA PT1000) from dried powdered samples by heating them to 950°C.

Specific surface area and pore volumes of samples were determined using N<sub>2</sub> gas adsorption-desorption isotherms at the temperature of liquid nitrogen (-196 °C) by using a Micrometrics ASAP 2020 instrument. Specific surface area was calculated based on the Brunauer-Emmett-Teller (BET) isotherm. Pore size distributions were calculated from desorption data using the Barrett-Joyner-Halenda (BJH) method.

## **2.4 Determination of ammonium removal efficiency**

NH<sub>4</sub><sup>+</sup> adsorption experiments for each prepared geopolymer specimen were conducted as batch experiments at room temperature (22°C). A model solution (NH<sub>4</sub><sup>+</sup> = 140 mg/l) whose pH was adjusted to 6.0 before experiments was prepared by dissolving NH<sub>4</sub>Cl (Merck) into ultrapure water. A constant dose of 5 g/L of MK-GP and a 24 h mixing time (in which equilibrium was reached) were used in every adsorption experiment. After mixing, MK-GP powder was separated by centrifuging and the supernatant was analyzed for NH<sub>4</sub><sup>+</sup> concentration using a flow injection analyzer (Foss-Tecator Fiastar 5000).

# **3. Results and discussion**

## **3.1 Characterization of the prepared metakaolin geopolymers**

The prepared geopolymer specimens used in experimental runs were labelled as MK-Na-N1 to MK-Na-N17 and MK-K-N1 to MK-K-N17 as shown in Table 2.

According to the XRD results (Fig. 1), there are no clear differences between the samples: all samples contain quartz (SiO<sub>2</sub>) and muscovite (KAl<sub>2</sub>(AlSi<sub>3</sub>O<sub>10</sub>)(OH)<sub>2</sub>). Additionally, all samples have an amorphous halo between approx. 25–35 °2θ which is associated with the unordered geopolymer structure and possibly unreacted metakaolin. Although there are no zeolite peaks present, it has been argued that the formation of nanocrystalline zeolites (crystals too small to cause X-ray diffraction) could take place during geopolymer formation [26].

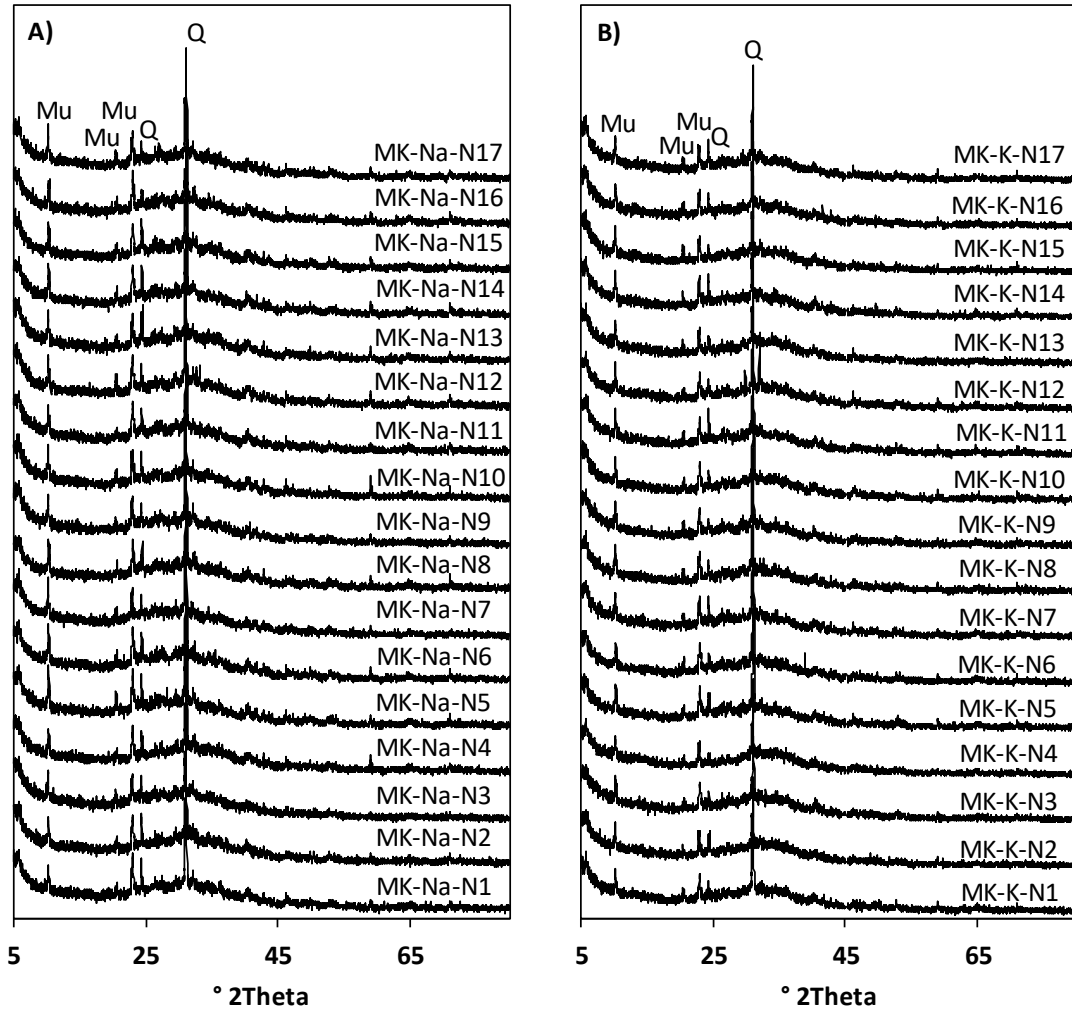


Fig. 1. X-ray diffraction patterns of A) Na-based and B) K-based MK-GPs. Mu = muscovite ( $\text{KAl}_2(\text{AlSi}_3\text{O}_{10})(\text{OH})_2$ ), Q = quartz ( $\text{SiO}_2$ ).

The elemental composition of the geopolymer specimens are shown in Table 3. The geopolymer structure is thought to consist of an irregular, i.e. amorphous, aluminosilicate network [27].  $\text{K}_2\text{O}$  in Na-based series originates from muscovite ( $\text{KAl}_2(\text{AlSi}_3\text{O}_{10})(\text{OH})_2$ ) which was present as an impurity in metakaolin. Other minor constituents ( $\text{SO}_3$ , Ti, and  $\text{Fe}_2\text{O}_3$ ) are related to amorphous impurity phases as there were no other phases than quartz and muscovite detected by XRD. The  $\text{SiO}_2/\text{Al}_2\text{O}_3$  molar ratio calculated from the results gives an approximation about the charge density of the aluminosilicate framework structure: the lower value is related to a more negative charge as the Al tetrahedron,  $[\text{AlO}_4]^-$ , are negatively charged [28]. However, also quartz and muscovite detected by XRD affect the  $\text{SiO}_2/\text{Al}_2\text{O}_3$  ratio in addition to the actual geopolymer framework structure and thus the  $\text{SiO}_2/\text{Al}_2\text{O}_3$  ratio in this case gives only a rough estimation about the charge density. There seems to be no clear linear correlation between the  $\text{SiO}_2/\text{Al}_2\text{O}_3$  molar ratio and  $\text{NH}_4^+$  removal capacity (shown in Tables 5 and 6). The  $\text{Na}_2\text{O}$  and  $\text{K}_2\text{O}$  concentrations indicate the amounts of exchangeable cations in geopolymers and in fact there is a rather clear linear correlation between  $\text{Na}_2\text{O}$  or  $\text{K}_2\text{O}$

and the  $\text{NH}_4^+$  adsorption capacity (Fig. 2). According to the literature, a higher Na/Al (or K/Al) ratio increases the formation of zeolitic phases similarly to increased water content [26, 29]. There were, however, no observable zeolite peaks present in the XRD results. The loss on ignition (LOI) value indicates the amount of water incorporated in the geopolymer structure. In addition, the calculated molar ratios of  $\text{M}_2\text{O}/\text{SiO}_2$  and  $\text{H}_2\text{O}/\text{M}_2\text{O}$  ( $\text{M} = \text{Na}$  or  $\text{K}$ ) are provided in Table 3. According to a review by Khale and Chaudhary [30], geopolymers have typically  $\text{SiO}_2/\text{Al}_2\text{O}_3$ ,  $\text{M}_2\text{O}/\text{SiO}_2$ , and  $\text{H}_2\text{O}/\text{M}_2\text{O}$  molar ratios within 3.3–4.5, 0.2–0.48 and 10–25, respectively. Some of the samples prepared in this study have values below or above the stated ranges. However, those typical ratios reported in the literature are related to optimizing mechanical properties such as compressive strength which are not a priority in the present study. Also, if waste materials are used in geopolymer preparation, the typical ranges are not necessarily applicable [30].

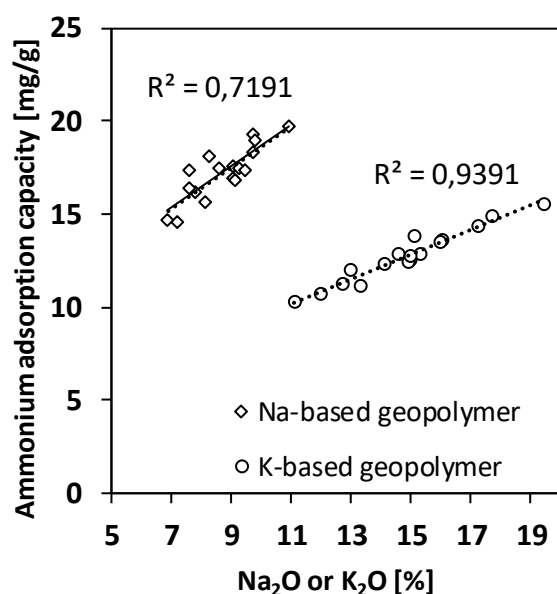


Fig. 2. The linear correlation between  $\text{Na}_2\text{O}$  or  $\text{K}_2\text{O}$  and the observed  $\text{NH}_4^+$  adsorption capacity.

Table 3. Elemental composition, loss on ignition (LOI), and calculated molar ratios of Na and K-based MK-GPs.

Sample	Elemental composition [%, w/w]							LOI [%, w/w]	Calculated molar ratios		
	Na <sub>2</sub> O	Al <sub>2</sub> O <sub>3</sub>	SiO <sub>2</sub>	SO <sub>3</sub>	K <sub>2</sub> O	Ti	Fe <sub>2</sub> O <sub>3</sub>		SiO <sub>2</sub> /Al <sub>2</sub> O <sub>3</sub> <sup>a</sup>	M <sub>2</sub> O/SiO <sub>2</sub> <sup>b</sup>	H <sub>2</sub> O/M <sub>2</sub> O <sup>c</sup>
MK-Na-N1	8.26	23.84	42.30	0.13	1.99	0.06	1.52	10.51	3.01	0.19	25.93
MK-Na-N2	9.70	23.72	40.96	0.11	1.95	0.05	1.45	12.55	2.93	0.23	20.71
MK-Na-N3	9.72	25.27	41.65	0.08	2.03	0.05	1.48	12.78	2.80	0.23	27.31
<b>MK-Na-N4</b>	<b>10.95</b>	<b>23.98</b>	<b>39.63</b>	<b>0.07</b>	<b>1.97</b>	<b>0.05</b>	<b>1.48</b>	<b>10.52</b>	<b>2.80</b>	<b>0.27</b>	<b>22.42</b>
MK-Na-N5	7.18	31.14	48.49	0.08	2.27	0.06	1.64	8.01	2.64	0.14	29.83
MK-Na-N6	7.76	28.80	45.06	0.07	2.23	0.06	1.61	9.02	2.66	0.17	25.89
MK-Na-N7	6.88	27.55	42.42	0.07	2.29	0.06	1.71	8.10	2.61	0.16	38.59
MK-Na-N8	9.07	29.78	45.29	0.09	2.23	0.06	1.62	9.15	2.58	0.19	27.07
MK-Na-N9	7.59	26.22	42.21	0.07	2.17	0.06	1.60	10.10	2.73	0.17	31.60
MK-Na-N10	8.62	24.99	40.37	0.11	2.04	0.07	1.54	11.79	2.74	0.21	25.89
MK-Na-N11	7.58	25.01	41.62	0.08	2.08	0.06	1.56	9.61	2.82	0.18	27.33
MK-Na-N12	9.05	26.59	41.89	0.07	2.15	0.06	1.60	8.15	2.67	0.21	28.18
MK-Na-N13	9.82	24.56	41.36	0.07	2.00	0.05	1.49	11.75	2.86	0.23	23.53
MK-Na-N14	8.15	30.45	46.59	0.08	2.27	0.06	1.63	6.90	2.60	0.17	28.35
MK-Na-N15	9.12	28.20	44.68	0.07	2.15	0.06	1.57	7.70	2.69	0.20	25.34
MK-Na-N16	9.27	28.62	45.43	0.07	2.15	0.06	1.58	7.39	2.69	0.20	24.93
MK-Na-N17	9.48	28.73	45.59	0.07	2.16	0.06	1.57	8.52	2.69	0.20	24.38
MK-K-N1	0.00	23.26	39.30	0.07	15.11	0.05	1.54	8.83	2.87	0.25	20.31
MK-K-N2	0.00	23.56	39.23	0.06	17.70	0.06	1.50	9.44	2.83	0.29	15.92
MK-K-N3	0.00	24.70	39.76	0.06	16.08	0.06	1.55	8.08	2.73	0.26	23.40
<b>MK-K-N4</b>	<b>0.00</b>	<b>24.90</b>	<b>39.85</b>	<b>0.06</b>	<b>19.47</b>	<b>0.05</b>	<b>1.50</b>	<b>11.43</b>	<b>2.72</b>	<b>0.31</b>	<b>17.39</b>
MK-K-N5	0.00	26.72	41.29	0.07	11.12	0.06	1.67	6.28	2.62	0.17	27.60
MK-K-N6	0.00	25.16	38.96	0.06	13.02	0.06	1.64	6.35	2.63	0.21	21.65
MK-K-N7	0.00	30.12	45.26	0.07	11.96	0.06	1.66	6.69	2.55	0.17	31.46
MK-K-N8	0.00	29.00	43.57	0.07	14.56	0.06	1.63	6.32	2.55	0.21	23.26
MK-K-N9	0.00	29.15	45.21	0.07	13.34	0.06	1.59	6.73	2.63	0.19	25.61
MK-K-N10	0.00	28.07	43.75	0.06	15.96	0.06	1.56	9.54	2.65	0.23	19.44
MK-K-N11	0.00	28.13	44.53	0.06	14.14	0.06	1.57	8.85	2.69	0.20	20.78
MK-K-N12	0.00	28.21	43.37	0.07	15.31	0.06	1.58	8.97	2.61	0.23	23.29
MK-K-N13	0.00	25.05	40.67	0.06	17.28	0.06	1.49	10.06	2.76	0.27	18.82
MK-K-N14	0.16	29.86	45.09	0.07	12.75	0.06	1.62	6.51	2.56	0.18	25.50
MK-K-N15	0.00	28.39	44.10	0.07	14.98	0.06	1.57	8.48	2.64	0.22	21.70
MK-K-N16	0.00	27.68	43.01	0.06	14.91	0.06	1.58	8.35	2.64	0.22	21.81
MK-K-N17	0.00	27.61	42.88	0.06	14.96	0.06	1.58	11.38	2.64	0.22	21.73

<sup>a</sup> = calculated from the XRF data, <sup>b</sup> = calculated from the XRF data, <sup>c</sup> = calculated from the XRF data and added water from hydroxide and silicate solutions. M = Na or K. The best-performing NH<sub>4</sub><sup>+</sup> adsorbents (MK-Na-N4 and MK-K-N4) are bolded.

The specific surface area and pore volume distribution between micro ( $d_0 < 2$  nm), meso ( $2 \text{ nm} < d_0 < 50$  nm) and macro ( $d_0 > 50$  nm) pores are shown in Table 4. The Na-based geopolymers have clearly lower specific surface area than K-based geopolymers. However, there is no linear correlation between the specific surface area and NH<sub>4</sub><sup>+</sup>



adsorption capacity in the results of the GPs. On the other hand, the average pore size is larger in the Na-based series. The reported aqueous ionic radii of Na, K, and  $\text{NH}_4^+$  are 0.235, 0.279, and 0.260 nm, respectively, which demonstrates that only micropores have a role in the adsorption phenomena [31]. As a trend, the specific surface area increases as the Si/Al ratio is increased: this is more evident in the K-based series.

Table 4. Specific surface areas and pore volume distributions of Na and K-based MK-GPs.

Sample	BET area [m <sup>2</sup> /g ]	Av. pore size [nm]	Micro pores [cm <sup>3</sup> /g]	Meso pores [cm <sup>3</sup> /g]	Macro pores [cm <sup>3</sup> /g]	Total volume [cm <sup>3</sup> /g]	Micro pores [%]	Meso pores [%]	Macro pores [%]
MK-Na-N1	37.8	26.8	0.002	0.116	0.134	0.252	0.61	46.12	53.27
MK-Na-N2	35.8	20.8	0.001	0.145	0.039	0.185	0.53	78.46	21.00
MK-Na-N3	23.7	26.0	0.001	0.080	0.072	0.153	0.56	52.38	47.05
<b>MK-Na-N4</b>	<b>19.3</b>	<b>30.3</b>	<b>0.000</b>	<b>0.106</b>	<b>0.040</b>	<b>0.147</b>	<b>0.26</b>	<b>72.28</b>	<b>27.46</b>
MK-Na-N5	31.6	24.6	0.001	0.106	0.088	0.195	0.50	54.44	45.06
MK-Na-N6	27.2	22.2	0.001	0.107	0.042	0.150	0.55	71.21	28.24
MK-Na-N7	19.1	31.2	0.001	0.064	0.083	0.148	0.38	43.45	56.16
MK-Na-N8	19.8	27.4	0.001	0.060	0.074	0.135	0.66	44.60	54.74
MK-Na-N9	28.3	26.2	0.001	0.095	0.087	0.184	0.66	51.92	47.42
MK-Na-N10	26.9	27.8	0.001	0.086	0.100	0.187	0.60	45.84	53.55
MK-Na-N11	32.5	28.2	0.001	0.115	0.112	0.227	0.40	50.37	49.23
MK-Na-N12	23.3	27.2	0.001	0.076	0.081	0.157	0.60	48.01	51.39
MK-Na-N13	28.5	29.9	0.001	0.089	0.121	0.212	0.46	42.10	57.44
MK-Na-N14	25.3	26.0	0.001	0.082	0.081	0.163	0.62	49.96	49.42
MK-Na-N15	25.0	32.1	0.001	0.079	0.119	0.199	0.39	39.73	59.88
MK-Na-N16	25.6	26.9	0.001	0.085	0.084	0.171	0.70	49.83	49.48
MK-Na-N17	23.4	28.9	0.001	0.078	0.089	0.168	0.58	46.67	52.75
MK-K-N1	94.0	15.1	0.002	0.309	0.044	0.355	0.40	87.20	12.40
MK-K-N2	110.0	12.5	0.002	0.300	0.040	0.342	0.50	87.90	11.60
MK-K-N3	88.0	17.9	0.002	0.364	0.030	0.396	0.40	92.00	7.60
<b>MK-K-N4</b>	<b>59.0</b>	<b>18.5</b>	<b>0.001</b>	<b>0.232</b>	<b>0.038</b>	<b>0.270</b>	<b>0.30</b>	<b>85.70</b>	<b>14.00</b>
MK-K-N5	80.0	13.9	0.002	0.245	0.030	0.277	0.60	88.70	10.70
MK-K-N6	72.0	13.4	0.002	0.201	0.037	0.240	0.80	83.80	15.40
MK-K-N7	64.0	17.0	0.001	0.247	0.021	0.268	0.40	91.90	7.70
MK-K-N8	52.0	17.8	0.001	0.193	0.037	0.231	0.50	83.60	15.80
MK-K-N9	81.0	15.8	0.002	0.290	0.026	0.318	0.50	91.20	8.30
MK-K-N10	68.0	14.7	0.002	0.204	0.044	0.249	0.60	81.80	17.60
MK-K-N11	84.0	13.8	0.002	0.254	0.033	0.289	0.60	88.00	11.30
MK-K-N12	60.0	18.0	0.001	0.240	0.027	0.268	0.40	89.60	10.00
MK-K-N13	82.0	15.2	0.002	0.263	0.048	0.312	0.50	84.10	15.50
MK-K-N14	64.0	16.0	0.001	0.221	0.034	0.257	0.40	86.20	13.40
MK-K-N15	73.0	15.5	0.002	0.224	0.056	0.282	0.60	79.70	19.80
MK-K-N16	79.0	14.8	0.002	0.233	0.057	0.292	0.80	79.70	19.50
MK-K-N17	60.0	18.8	0.000	0.225	0.058	0.282	0.00	79.60	20.40

The best-performing NH<sub>4</sub><sup>+</sup> adsorbents (MK-Na-N4 and MK-K-N4) are in bold. Micropores: d<sub>0</sub> < 2 nm, mesopores 2 < d<sub>0</sub> < 50 nm, macropores d<sub>0</sub> > 50 nm

### **3.2 Optimization of geopolymer preparation conditions for ammonium removal**

The experimental results for  $\text{NH}_4^+$  adsorption capacities obtained with CCF designs for Na and K-based MK-GPs are shown in Tables 5 and 6. The best  $\text{NH}_4^+$  removal was achieved with samples MK-Na-N4 and MK-K-N4. The Na-based geopolymers had 27–48% higher  $\text{NH}_4^+$  removal capacity than the K-based geopolymers. It should be noted that the reported capacities do not represent the theoretical maximum adsorption capacity but the capacity obtained within the experimental conditions (5 g/L adsorbent dose, 140 mg/L initial  $\text{NH}_4^+$  concentration, and 24 h mixing time). The maximum adsorption capacity of the best material (MK-Na-N4) in model solutions was determined to be 31.79 mg/g in another study [32]. This is above the typical maximum  $\text{NH}_4^+$  adsorption capacities of natural zeolites and is exceeded only by few synthetic zeolites reported in the literature [18].

Table 5. The results of the  $\text{NH}_4^+$  removal tests with Na-based MK-GPs.

Experimental run (sample)	Factor/level			Observed $\text{NH}_4^+$ adsorption capacity [mg/g] experiment 1	Observed $\text{NH}_4^+$ adsorption capacity [mg/g] experiment 2
	A: NaOH [g]	B: Na silicate [g]	C: Metakaolin [g]		
MK-Na-N1	-1 (6.24)	-1 (7.95)	-1 (50)	18.1	18.2
MK-Na-N2	+1 (8.67)	-1 (7.95)	-1 (50)	19.2	19.3
MK-Na-N3	-1 (6.24)	+1 (9.72)	-1 (50)	18.3	18.3
<b>MK-Na-N4</b>	<b>+1 (8.67)</b>	<b>+1 (9.72)</b>	<b>-1 (50)</b>	<b>19.7</b>	<b>19.7</b>
MK-Na-N5	-1 (6.24)	-1 (7.95)	+1 (80)	14.5	14.7
MK-Na-N6	+1 (8.67)	-1 (7.95)	+1 (80)	16.3	16.0
MK-Na-N7	-1 (6.24)	+1 (9.72)	+1 (80)	14.7	14.7
MK-Na-N8	+1 (8.67)	+1 (9.72)	+1 (80)	16.5	17.3
MK-Na-N9	-1 (6.24)	0 (8.84)	0 (65)	16.5	16.3
MK-Na-N10	+1 (8.67)	0 (8.84)	0 (65)	17.3	17.7
MK-Na-N11	0 (7.455)	-1 (7.95)	0 (65)	17.3	17.5
MK-Na-N12	0 (7.455)	+1 (9.72)	0 (65)	17.7	17.4
MK-Na-N13	0 (7.455)	0 (8.84)	-1 (50)	19.1	18.8
MK-Na-N14	0 (7.455)	0 (8.84)	+1 (80)	15.7	15.7
MK-Na-N15	0 (7.455)	0 (8.84)	0 (65)	16.6	17.1
MK-Na-N16	0 (7.455)	0 (8.84)	0 (65)	17.4	17.5
MK-Na-N17	0 (7.455)	0 (8.84)	0 (65)	17.3	17.4

Table 6. The results of the  $\text{NH}_4^+$  removal tests with K-based MK-GPs.

Experimental run (sample)	Factor/level			Observed $\text{NH}_4^+$ adsorption capacity [mg/g] experiment 1	Observed $\text{NH}_4^+$ adsorption capacity [mg/g] experiment 2
	A: KOH [g]	B: K silicate [g]	C: Metakaolin [g]		
MK-K-N1	-1 (8.29)	-1 (8.07)	-1 (50)	13.9	13.7
MK-K-N2	+1 (11.33)	-1 (8.07)	-1 (50)	14.9	14.9
MK-K-N3	-1 (8.29)	+1 (9.86)	-1 (50)	13.6	13.7
<b>MK-K-N4</b>	<b>+1 (11.33)</b>	<b>+1 (9.86)</b>	<b>-1 (50)</b>	<b>15.3</b>	<b>15.7</b>
MK-K-N5	-1 (8.29)	-1 (8.07)	+1 (80)	10.1	10.5
MK-K-N6	+1 (11.33)	-1 (8.07)	+1 (80)	11.9	12.1
MK-K-N7	-1 (8.29)	+1 (9.86)	+1 (80)	10.7	10.7
MK-K-N8	+1 (11.33)	+1 (9.86)	+1 (80)	13.3	12.5
MK-K-N9	-1 (8.29)	0 (8.965)	0 (65)	10.9	11.3
MK-K-N10	+1 (11.33)	0 (8.965)	0 (65)	13.5	13.5
MK-K-N11	0 (9.81)	-1 (8.07)	0 (65)	12.5	12.2
MK-K-N12	0 (9.81)	+1 (9.86)	0 (65)	12.9	17.5 <sup>a</sup>
MK-K-N13	0 (9.81)	0 (8.965)	-1 (50)	14.4	18.2 <sup>a</sup>
MK-K-N14	0 (9.81)	0 (8.965)	+1 (80)	11.5	10.9
MK-K-N15	0 (9.81)	0 (8.965)	0 (65)	12.9	12.1
MK-K-N16	0 (9.81)	0 (8.965)	0 (65)	12.7	12.1
MK-K-N17	0 (9.81)	0 (8.965)	0 (65)	13.1	12.3

<sup>a</sup> = Outlier excluded from the experimental data.

Quadratic models were fitted to the experimental data using the multiple linear regression technique (MLR). The significance of the models was tested by means of analysis of variance (ANOVA). The ANOVA results for the response surface quadratic models are summarized in Tables 7 and 8. As an overview, the goodness of fit ( $R^2$ ) and goodness of prediction ( $Q^2$ ) for both models were very good.

The model for Na-based MK-GP is discussed first. The important diagnostic tools,  $R^2$  and  $Q^2$ , exhibited high values: 0.979 and 0.959, respectively. Hence, the model fitted very well to the experimental data and the model also had a very good predictive power. The model coefficients are presented in Fig. 3. There are some insignificant two-factor interaction terms in the model that could be removed. However, the regression model is statistically significant ( $p < 0.05$ ) and there is no lack of fit (0.641, Table 7). The normal probability plot of residuals shows that there are no outliers in the experimental data but that two experiments deviated to some extent (Fig. 4). The deviations were MK-Na-N8 experiment 1 and MK-Na-N13 experiment 1 (see Table 6). However, they were not excluded from the experimental data.

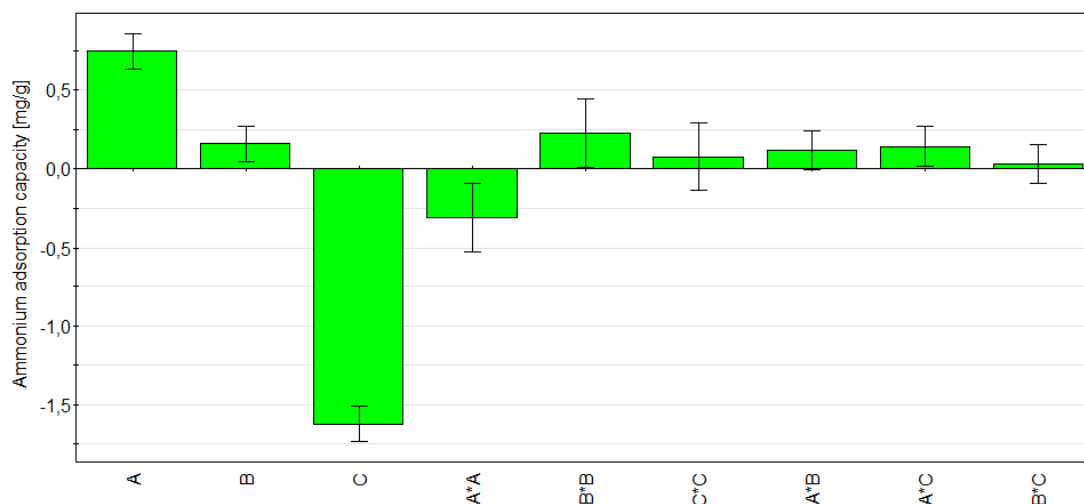


Fig 3. Scaled and centered regression coefficients for the model of the Na-based MK-GPs.

Table 7. ANOVA for the response surface quadratic model for Na-based MK-GP.  $R^2 = 0.979$  and  $Q^2 = 0.959$ .

Source of variation	Degree of freedom	Sum of squares	Mean square	F value	p value
Model	9	65.416	7.2685	123,203	$7.108 \times 10^{-18}$
Residual	24	1.4159	0.058996		
Lack of fit	5	0.21620	0.043239	0.684795	0.641
Pure error	19	1.1997	0.063142		
Total corrected	33	66.832	2.0252		

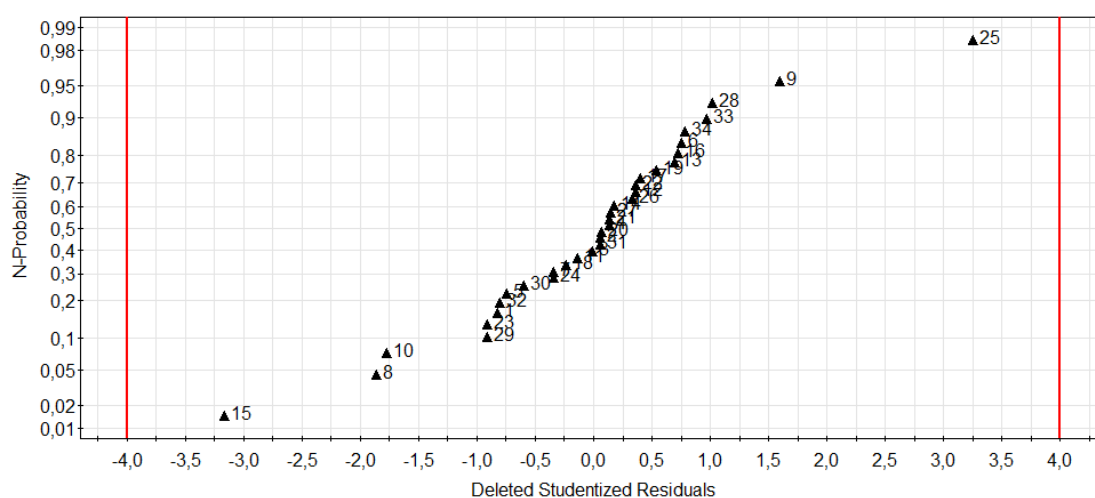


Fig 4. Normal probability plot of residuals for Na-based MK-GPs.

The obtained regression model for the K-based MK-GPs was also very good ( $R^2 = 0.964$  and  $Q^2 = 0.933$ ). The model coefficients are presented in Fig. 5. Again, similarly as with the Na-based series, there are some insignificant two-factor interaction terms in the model that could be removed. However, according to the ANOVA (Table 8), the model was significant and there was no lack of fit. The normal probability plot (Fig. 6) of residuals showed two outliers in the experimental data (shown in Table 6) which were excluded from the data analysis. The observed main effects were similar to that of Na-based MK-GPs.

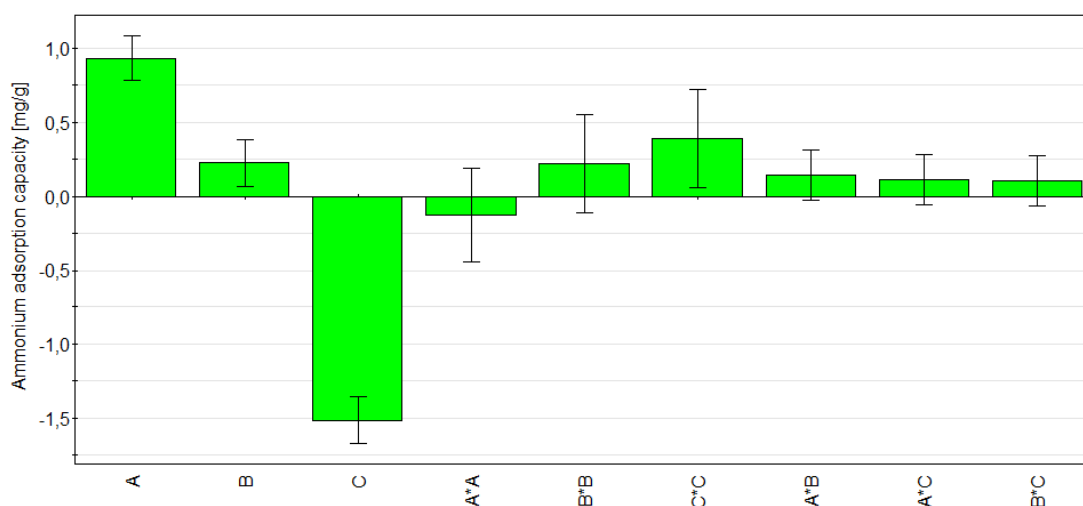


Fig 5. Scaled and centered regression coefficients for the model of the K-based MK-GPs.

Table 8. ANOVA for the response surface quadratic model for K-based MK-GP.  $R^2 = 0.964$  and  $Q^2 = 0.933$ .

Source of variation	Degree of freedom	Sum of squares	Mean square	F value	p value
Model	9	64.187	7.1319	66.313	$7.364 \times 10^{-14}$
Residual	22	2.3661	0.10755		
Lack of fit	5	0.52727	0.10545	0.97495	0.461
Pure error	17	1.8388	0.10816		
Total corrected	32	66.553	2.1469		

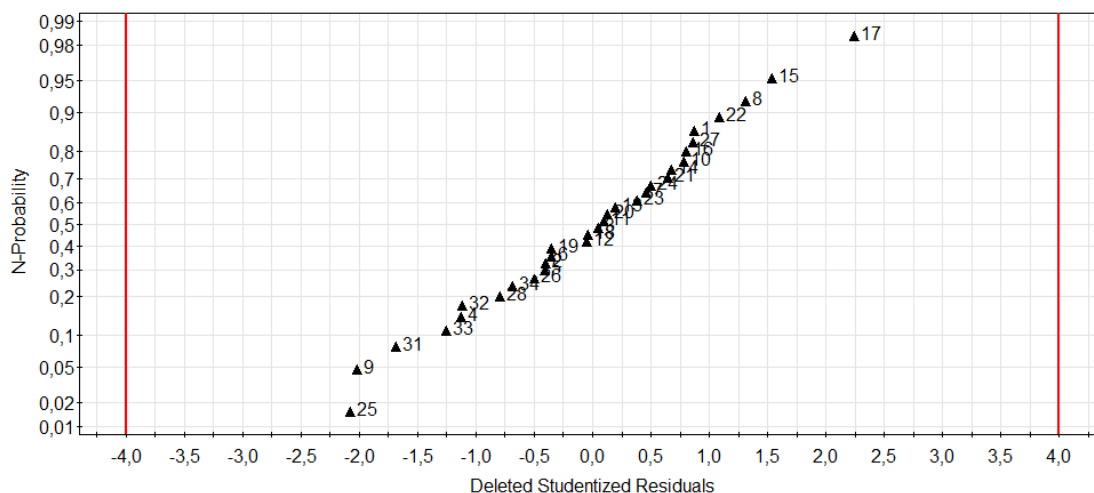


Fig 6. Normal probability plot of K-based MK-GP residuals.

The highest experimental  $\text{NH}_4^+$  adsorption capacity (19.7 mg/g and 15.5 mg/g as an average of two repetitions for Na and K-based series, respectively) was achieved using the highest amount of hydroxide (8.67 or 11.33 g of NaOH or KOH, respectively), the highest amount of silicate (9.72 or 9.86 g of Na or K silicate, respectively) and the lowest amount of metakaolin (50 g) in the MK-GP preparation (Tables 5 and 6). The predicted values by of  $\text{NH}_4^+$  adsorption capacity were in good agreement with the experimental results (Fig. 7 and 8). These observed effects are most likely due to the more efficient conversion of metakaolin into geopolymer: metakaolin very low  $\text{NH}_4^+$  adsorption capacity [18]. Increased amount of soluble silica and hydroxide increase the degree of geopolymerization through an improved dissolution of precursor alumino-silicate [33, 34]. On the other hand, decreasing the amount metakaolin minimizes the amount of unreacted metakaolin in the final product. As the ammonium removal was observed as adsorption capacity per unit weight (mg/g), the amount of unreacted metakaolin directly reduces the capacity. Finally, the reason why the Na based series resulted into higher  $\text{NH}_4^+$  removal than the K based series is not as clear. It has been noted that  $\text{Na}^+$  results into more ordered framework than  $\text{K}^+$  which indicates that the Na based series might have more favourable void structure for  $\text{NH}_4^+$  adsorption [2].



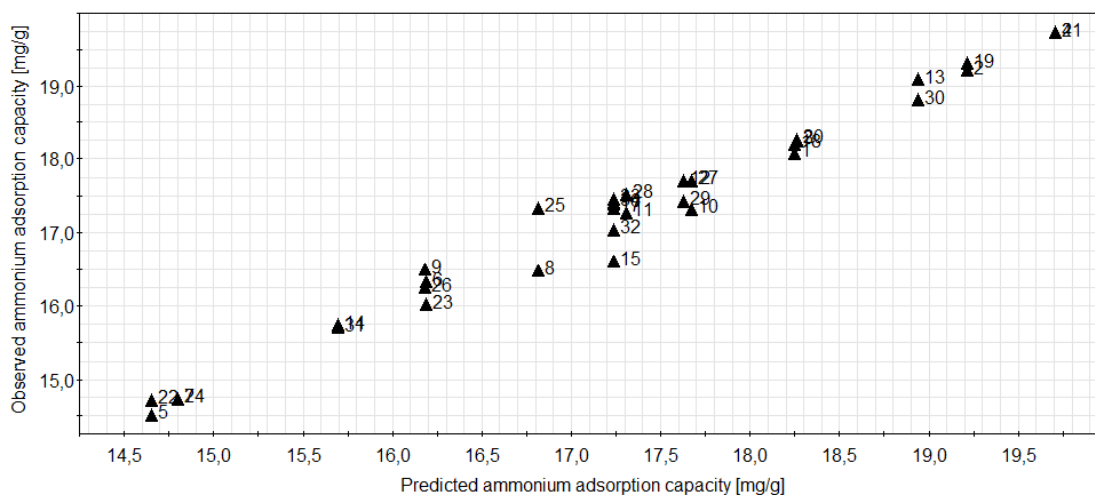


Fig. 7. Observed response vs. model predicted response plot for Na-based MK-GPs.

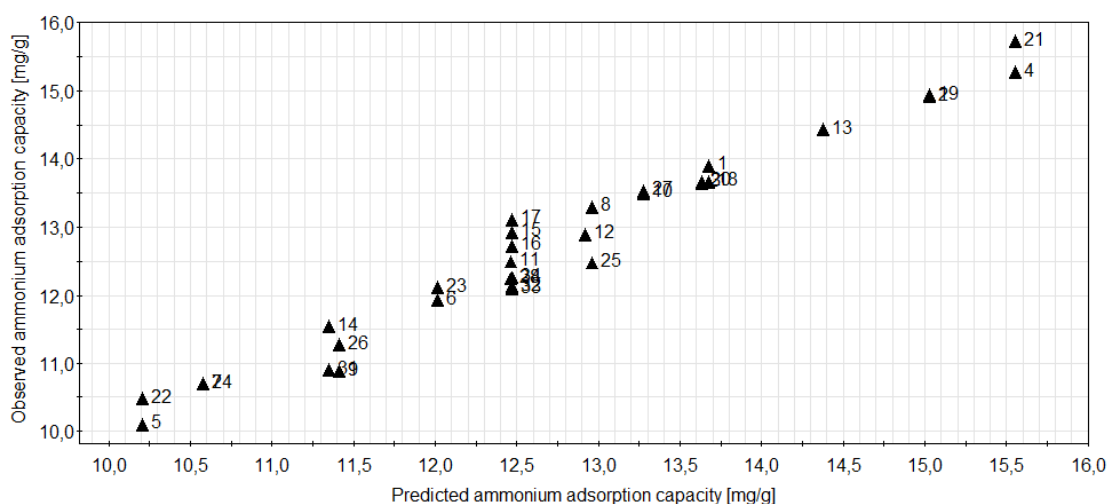


Fig. 8. Observed response vs. model predicted response plot for K-based MK-GPs.

The response surface plots (Figs. 9 and 10) show the effects of the amounts of hydroxide and metakaolin on the  $\text{NH}_4^+$  adsorption efficiency. The third factor (the amount of silicate) was fixed at a high level (see Table 1) since it gave the best results in the experiments. According to the fitted models, an even higher  $\text{NH}_4^+$  adsorption capacity could be possibly obtained by further increasing the amounts of hydroxide or silicate or by decreasing the amount metakaolin. However, viscosity of the alkaline solution increases if the weight percentage of solids is increased [35]. Additionally, the  $\text{SiO}_2/\text{M}_2\text{O}$  ( $\text{M} = \text{Na}$  or  $\text{K}$ ) molar ratio of the alkaline solution also affects the viscosity and in fact there is a minimum viscosity area in terms of  $\text{SiO}_2/\text{M}_2\text{O}$  which gets narrower as the percentage of solids increases [35]. The optimum  $\text{SiO}_2/\text{Na}_2\text{O}$  molar ratio of alkaline solution would be approx. 1.8 in terms of viscosity [35]. In the present study, the  $\text{SiO}_2/\text{Na}_2\text{O}$  molar ratio (in the Na-based series) of alkaline solution was 0.27–0.57 and it was noticed that if the alkaline solutions were allowed to stand several days, crystals were formed especially in those alkaline solutions containing more concentrated

hydroxide. One advantage of a K-based alkali solution is significantly lower viscosity compared to a Na-based alkali solution at the same concentration [36]. Subsequently, the precipitate formation when using KOH and K silicate is not as severe. Due to the aforementioned reasons, the NaOH or KOH concentration cannot be increased arbitrarily. The amount of metakaolin, on the other hand, cannot be varied outside the current range or the workability of the geopolymer paste becomes difficult.

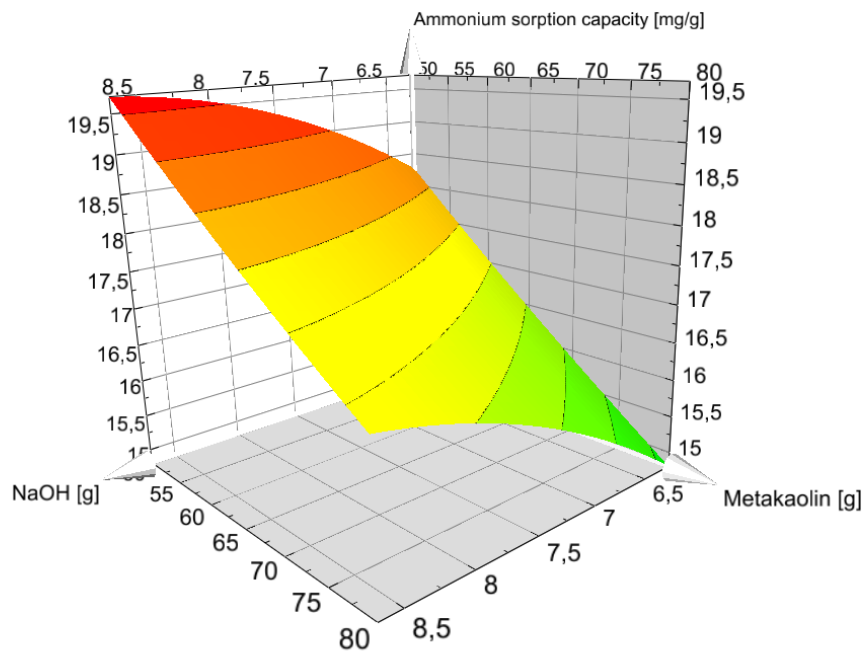


Fig. 9. Response surface plot of the NaOH and metakaolin amounts (in grams) on  $\text{NH}_4^+$  adsorption capacity at a sodium silicate mass of 9.72 g.

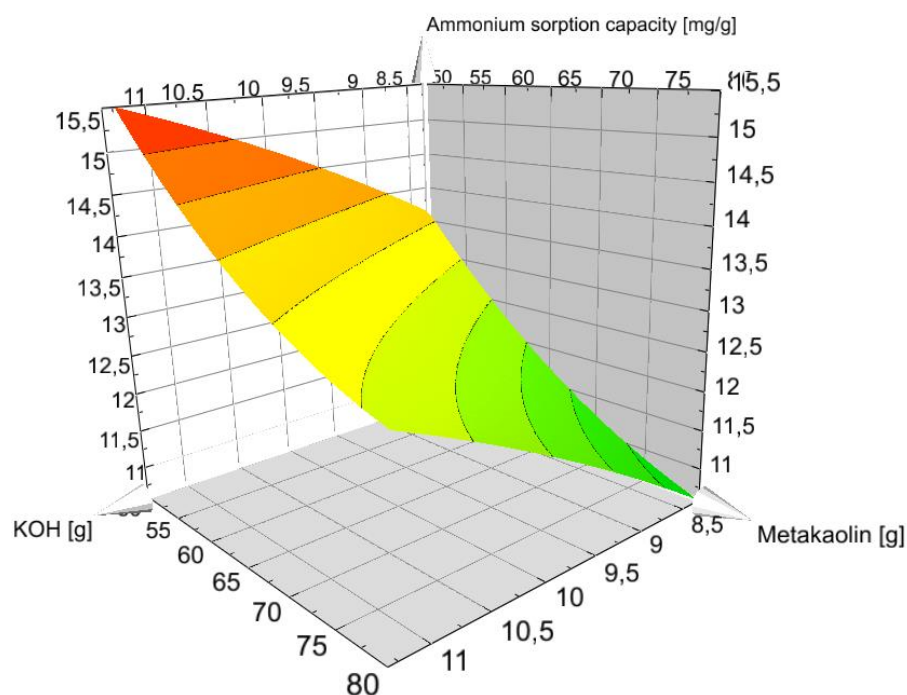


Fig. 10. Response surface plot of the KOH and metakaolin amounts (in grams) on  $\text{NH}_4^+$  adsorption capacity at a potassium silicate mass of 9.86 g.

### 3 Conclusions

The aim of this study was to find the optimum composition for metakaolin geopolymer in terms of  $\text{NH}_4^+$  adsorption capacity. The response surface methodology based on a face centered central composite design was used to evaluate the effects of and to find optimum values for three factors: the amounts of hydroxide, silicate, and metakaolin used for the geopolymer preparation. The  $\text{NH}_4^+$  adsorption capacity was used as the response function. Furthermore, the effect of charge balancing cation (i.e.  $\text{K}^+$  or  $\text{Na}^+$ ) was studied by conducting all experiments with sodium and potassium hydroxide and silicate.

The following main conclusions can be drawn:

- The highest  $\text{NH}_4^+$  removal with metakaolin geopolymer was achieved when maximizing the amounts of NaOH and Na silicate and minimizing the amount of metakaolin in the preparation of geopolymer. This was most likely due to the more efficient conversion of metakaolin into geopolymer by adjusting the aforementioned parameters.
- Sodium-based metakaolin geopolymers had 27–48% higher  $\text{NH}_4^+$  adsorption capacity than potassium-based metakaolin geopolymers. There was no conclusive explanation for this observation but it could be related to the void

structure: Na<sup>+</sup> has been reported to result a more ordered alumino-silicate framework than K<sup>+</sup>. All samples were still X-ray amorphous.

- According to the fitted models, the maximum adsorption capacity seemed to be outside the studied range of factors (i.e., an even higher amount of NaOH and Na silicate and a lower amount of metakaolin would have been required).
- In practice, the amounts of NaOH or Na silicate cannot be further increased due to the precipitation tendency of a highly concentrated alkali solution with the SiO<sub>2</sub>/M<sub>2</sub>O (M = Na or K) molar ratio much higher or lower than 1.8. The amount of metakaolin cannot be changed outside the studied range or the workability of geopolymer paste becomes poor. According to the literature, the potassium silicate solutions are not as prone to precipitation as sodium silicate solutions.

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