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INTENSIFICATION OF UV-C TREATMENT TO REMOVE EMERGING CONTAMINANTS BY UV-C/H₂O₂ AND UV-C/S₂O₈²⁻: SUSCEPTIBILITY TO PHOTOLYSIS AND INVESTIGATON OF ACUTE TOXICITY

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16 **GRAPHICAL ABSTRACT**

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18 ABSTRACT

In this study, the degradation of four emerging contaminants (losartan potassium) 19 (LP), furosemide (FRSM), caffeine (CAF), and carbendazim (CBZ) under UV-C, 20 UV-C/H₂O₂, and UV-C/S₂O_{8²⁻ was investigated. A comparative evaluation of the} 21 efficiency of UV-C/H₂O₂ and UV-C/S₂O_{8²⁻ in the degradation of these target CECs} 22 23 has not yet been reported. Moreover, target compounds were submitted to UV-24 C/AOPs individually in pure water and their simultaneous degradation was investigated in real surface water. Evolution of the acute toxicity of each 25 26 compound during treatment was evaluated using Alivibrio fischeri. Quantum yields were determined for LP (0.011 to 0.016), FRSM (0.024 to 0.092), CAF 27 (0.0007 to 0.0009), and CBZ (0.0016 to 0.0036) at different pH values. UV-28 29 C/H₂O₂ and UV-C/S₂O₈² achieved more than 98% removal of all compounds within 600 mJ cm⁻², and pseudo-fist-order kinetic constants (k'_{app}) for the 30

degradation reactions were up to seven times higher in the presence of these 31 oxidants when compared to k'app values obtained for UV-C photolysis. k'app 32 measured for UV-C/H₂O₂ were higher than those calculated for UV-C/S₂O₈²⁻ 33 except in the case of LP. Acute toxicity analysis suggested the formation of toxic 34 intermediates during the UV-C photolysis of LP and FRSM, and the degradation 35 of LP via UV-C/S₂O_{8²⁻} also enhaced acute toxicity although electric energy 36 efficiency per order identified UV-C/S₂O₈² as the most efficient process for the 37 removal of this compound. Finally, different transformation products obtained 38 during the degradation of caffeine under the different UV-C AOPs suggested that 39 distinct degradation routes were involved in each treatment tested. 40

41

Keywords: advanced oxidation processes, persulfate, UV-C process, quantumyield, contaminants of emerging concern

45 1. Introduction

After the scientific community raised awareness regarding the presence of contaminants of emerging concern (CECs) in different water resources (i.e. drinking water, groundwater, surface water, and wastewater) these compounds have been intensively studied over the past two decades. Therefore, many technologies have been developed for the removal of CECs from these matrices.

Advanced oxidation processes (AOPs) have proven to be effective methods for the degradation of CECs [1]. AOPs incorporating UV-C irradiation (UV-C AOPs) are attractive alternatives within this category [2, 3], because the UV-C reactors already being used worldwide in water and wastewater treatment plants could be easily adapted for these processes [4].

Photoperoxidation (UV-C/H₂O₂) is one of the most disseminated AOPs [5], wherein H₂O₂ undergoes UV-C photolysis (λ =254 nm) and is cleaved into two hydroxyl radicals (HO•) [6]. HO• presents a high redox potential (E⁰= 1.8–2.7 V), thus being highly reactive and non-selective [7]. In addition, the UV-C/H₂O₂ process does not require pH adjustment, simplifying operational requirements in comparison to those involved in other AOPs such as Fenton and photo-Fenton [8, 9].

Most of the studies using UV-C/H₂O₂ to remove CECs from water have used pure solutions of target compounds in synthetic matrices [6, 10-12]. Meanwhile, in real matrices containing natural organic matter (NOM), inorganic ions (HCO₃, Cl⁻, NO₃⁻ , and SO₄²⁻), and dissolved oxygen (DO), UV-C/H₂O₂ reactions may be disturbed due to quenching of HO• [13], thus reducing the process efficiency. There has,

thus, been increased interest in alternative systems that employ strongly reactive
yet selective radicals, such as the sulfate radical (SO₄-•) [14].

In irradiated systems, SO_4^{-1} ($E^0 = 2.55 - 3.1$ V) is formed when persulfate (PS, 70 $S_2O_8^{2-}$) or peroxymonosulfate (PMS, SO_5^{2-}) are cleaved under UV-C (254 nm) 71 irradiation [15]. SO₄-• reacts primarily via an electron transfer mechanism, and is, 72 thus, more selective and resistant than HO• in the presence of matrix constituents 73 such as NOM and inorganic ions [16]. In addition, SO₄-• is not as easily influenced 74 by carbonate ions (HCO₃-) due to the lower rate constant of the reaction between 75 SO_4^{-1} and HCO_3^{-1} (2.6 to 9.1 x $10^6 M^{-1} s^{-1}$) compared to that of the reaction between 76 HO• and HCO₃⁻ ($10^7 M^{-1} s^{-1}$) [6, 14, 17-20]. The removal of CECs via UV-C/H₂O₂ 77 and UV-C/S2O82- varies according to the chemical structure of the compound 78 involved and as a consequence of the different reaction mechanisms promoted 79 by each radical [2, 21, 22]. 80

Toxic intermediates may be generated during UV-C AOPs [23], and appropriate 81 treatment conditions for the simple removal of target compounds may not 82 effectively eliminate their toxic effects [24]. Therefore, it is essential to follow the 83 84 evolution of the toxicity of compounds during their treatment by UV-C AOPs in order to comprehensively understand treatment efficiency [25], especially with 85 regard to UV-C/S₂O_{8²⁻, for which only a few studies have investigated toxicity} 86 87 evolution [26, 27]. In addition, since in industrial applications these advanced treatments would not be utilized to achieve complete mineralization of CECs, it is 88 necessary to investigate the evolution of toxicity resulting from the degradation of 89 90 various harmful CECs present in environmental samples, as well as to identify any intermediates and/or byproducts of their degradation processes. 91

Considering the vast diversity of emerging contaminants present in surface water, 92 four CECs were chosen as representative compounds for different classes of 93 contaminants because of their environmental relevance as they have been 94 increasingly consumed and consequently detected in surface water worldwide. 95 Losartan potassium (LP) and furosemide (FRSM) represent pharmaceutical 96 drugs. These compounds are widely prescribed to hypertensive patients 97 worldwide and have been detected in environmental matrices in various locations 98 [28-33], especially in developing countries where sanitary conditions are 99 inadequate [34]. Caffeine (CAF) was chosen due to its regular occurrence in 100 101 surface water and drinking water resources, for which it was recently proposed as an urban pollution tracer [35-37]. The fungicide carbendazim (CBZ), which has 102 103 been detected in surface water around the world and is known for its toxicity, 104 represents the diverse group of agrochemicals [36, 38, 39].

In this context, the goals of this study were to assess the susceptibility LP, FRSM, CAF and CBZ to UV-C photolysis; to evaluate the performance of UV-C/S₂O₈²⁻ and UV-C/H₂O₂ in the degradation of each target compound individually in pure water as well as that of the four compounds in conjunction in pure water and real surface water; and to investigate the impact of each UV-C AOP on acute toxicity.

110 2. Material and Methods

111 2.1 Determination of quantum yields

112 LP, FRSM, CAF, and CBZ were purchased from Sigma-Aldrich. Table S1 113 (Supplementary Material) shows the chemical structures and some 114 physicochemical properties of each of the four CECs. Figure S1 shows the UV-115 Vis absorption spectra of the CECs at the natural pH of each solution.

Experiments for the determination of quantum yields (ϕ) were conducted in a UV-116 C bench reactor (volume 0.0035 L, pathway length 1 cm⁻²) equipped with a low-117 pressure mercury-xenon lamp (LightningCure LC8, Hamamatsu City, Japan) 118 under constant agitation by using a magnetic stirrer. Lamp intensity (I_0) was 119 determined prior to experiments using H₂O₂ ($I_0 = 2.54 \text{ Jm}^2 \text{ s}^{-1}$) and atrazine ($I_0 =$ 120 2.14 J m⁻² s⁻¹) as actinometers [40, 41]. A UV filter (254 nm; Semrock MaxLamp) 121 was placed at the light source. Initial concentrations of LP, FRSM, CAF, and CBZ 122 were 2.2, 3.0, 5.2, and 5.5 µM, respectively. Quantum yields were calculated by 123 quantifying the decay of each compound when exposed to light at pH = 3.0, the 124 125 natural pH of the solution (6.0 for LP, 5.5 for FRSM, 5.8 for CAF, and 7.1 for CBZ), and at pH = 9. The pH was adjusted using 0.01 M HCl or 0.01 M NaOH 126 solutions. 127

The photolysis coefficient (C_p) was calculated for each of the target compounds. C_p is defined as the product of the quantum yield (Φ_{254nm}) and the molar attenuation coefficient (ξ_{254nm}) of a substance, and can be calculated according to Equations 1 and 2 [4]:

132
$$k_d = (\Phi_{254nm} \times \xi_{254nm} \times 2302)/U = (Cp \times 2302/U)$$
 (Eq. 1)

133
$$Cp = (k_d \times U)/2302$$
 (Eq. 2)

where k_d is the fluence-based pseudo-first-order rate constant (units J⁻¹ cm⁻²), *U* is the energy per mole of photons at 254 nm (4.72 x 10⁵ J Einstein⁻¹), and 2302 is a factor used for unit conversion purposes (base 10 to base e, and mJ to J).

137 2.2 High-Performance Liquid Chromatography analyses

138 A liquid chromatograph equipped with a UV detector (Agilent 1260 Infinity II

series, UV and diode array detector equipped with a 60 mm high-sensitivity cell) 139 was used for the quantification of CECs. The separation was performed on C₁₈ 140 columns (Poroshell 120 EC-C18 (3 x 50 mm, internal diameter 2.7 µm) followed 141 by Poroshell HPH-C18 (4.6 x 150 mm, internal diameter 2.7 µm) at a flow rate of 142 0.5 mL min⁻¹. Ultra-pure water (40%) and MeOH (60%; MERCK HPLC grade, 143 98% purity), both containing 0.1% formic acid (SIGMA-ALDRICH HPLC grade, 144 145 98% purity), was used as the mobile phase for LP and FRSM, adapting previously described procedures [42]. Both LP and FRSM were monitored at λ =240 nm. 146 147 Methods adapted from those described by the USA Environmental Protection Agency (EPA) [43, 44] were used for the quantification of CAF (MeOH/H₂O 30/70 148 (v/v), 273 nm) and CBZ (MeOH/H₂O 50/50 (v/v); 285 nm). 149

150 2.3 Degradation of target compounds by UV-C AOP

UV-C, UV-C/H₂O₂, and UV-C/S₂O_{8²⁻} treatments were performed in a 2 L 151 cylindrical bench photo-reactor equipped with a low-pressure mercury vapor lamp 152 emitting monochromatic radiation at 253.7 nm (Heraeus GPH212T5L/4, 10 W) in 153 154 the axial position. The optical pathway (1.7 cm) was calculated according to the method developed by Beltran et al. (1995) [45]. Incident photonic flux (I₀) was 155 determined via actinometry experiments using H₂O₂ and atrazine as actinometers 156 [40, 41], the results of which indicated an I_0 of 2.41 J m⁻² s⁻¹. The reactor was 157 coupled to a cooling system, and temperature was kept constant at 20 °C during 158 reactions. 159

The UV-C lamp was pre-heated for 20 minutes before each reaction. Once the solution temperature was stabilized at 20 °C, H₂O₂ (commercial grade, 39%) or sodium persulfate (Na₂SO₈, Aldrich) were added to the solution at a concentration

of 10^{-3} M (molar ratio of H₂O₂ or S₂O₈²⁻: target substance 20:1 for CAF, LP, and FRSM, and 32:1 for CBZ). Samples were withdrawn during the reactions for quantification of the target compounds using HPLC, total organic carbon (TOC; TOC-VCSH Total Carbon Analyzer, Shimadzu), and residual H₂O₂ or persulfate, according to previously described procedures [46]. All conditions were tested in duplicate, and the pH was monitored during reactions.

In order to assess the influence of natural scavengers, namely inorganic ions 169 (HCO₃⁻, NO₃⁻, PO₄³⁻) and NOM, on the degradation of CECs via UV-C, UV-170 C/H₂O₂, and UV-C/S₂O₈²⁻, reactions were performed in surface water and ultra-171 172 pure water each containing all four target compounds. Both matrices were spiked with a solution containing a mix of the four compounds such that the final 173 concentration of each compound was 10 μ M (total CEC₀ concentration = 40 μ M). 174 175 The surface water (SW) used in these experiments was sampled from the Lys River at Aire sur la Lys, France. 176

177 2.4 Acute toxicity assays

Acute toxicity analyses were performed using the Microtox® method (Model 500 178 Analyzer SDI) (ISO 11348-3:2007) on samples withdrawn during UV-C photolysis 179 and the UV-C AOP processes performed in the UV-C reactor, as described 180 181 previously [47]. Allivibrio fischeri was exposed to samples diluted to different 182 degrees, luminescence was measured after 5, 15, and 30 min of exposure, and relative inhibition (EC₅₀, %) was obtained and converted to acute toxicity units 183 $(a.T.u.; = 100/EC_{50})$. According to the method employed, samples were 184 185 considered toxic when the a.T.u. value was above 1.2 ($EC_{50} > 81.9\%$). Catalase (Synth®, 460 mg L⁻¹ in 0.04 M phosphate buffer) and ascorbic acid (Merck, 440 186

mg L⁻¹) solutions were used as quenching agents for the consumption of residual
hydrogen peroxide and persulfate present in the samples, respectively [48, 49].
Neither of these reagents are toxic to *Allivibrio fischeri,* as previously reported
[49] and as confirmed experimentally by blank tests. The pH was adjusted (to
6.5–7.5) prior to toxicity analysis.

192 2.5 Transformation products (TPs)

The samples withdrawn during UV-C and UV-C/AOP treatments were analyzed 193 injection high-resolution electrospray ionization (ESI)-mass 194 via direct 195 spectrometry (Bruker micrOTOF-QII) in negative mode for LP and FRSM, and in positive mode for CAF and CBZ. In order to increase the signal, formic acid was 196 added to the CAF and CBZ samples, and ammonium hydroxide was added to 197 198 the FRSM and LP samples (both at concentrations at 0.1%). A blank sample containing water and formic acid or ammonium hydroxide was analyzed before 199 200 each measurement. The transformation products (TPs) obtained from the original substances were proposed by considering two different strategies: a structure 201 showing the exact mass detected by the instrument; or simpler structures 202 203 considering oxidative radical attack and the energy required to break specific chemical bonds in the original molecule. 204

205 3. Results and Discussion

3.1 Determination of quantum yields

207

Figure 1 shows the UV-C photolysis of each target compound at different pH values, and Table 1 presents the quantum yields and C_p values obtained at acidic (pH = 3.0), natural (pH of solution without adjustment), and basic (pH = 9.0) pH.

211

Figure 1. Photolysis (UV-C_{254nm}) of LP (2.2 μ M), FRMS (3.0 μ M), CAF (5.2 μ M), and CBZ (5.5 μ M) in ultrapure water at acidic, natural (non-adjusted), and basic pH ($I_0 = 2.54$ J m⁻² s⁻¹, volume 3.5 mL) as a function of incident energy per area (mJ cm⁻²).

216

Table 1 – Quantum yields and photolysis coefficients (C_p) obtained for each compound at 254 nm at different pH values.

	Φ _{254 nm} (mol Einstein ⁻¹)	Cp 254 nm(L Einstein ⁻¹ cm ⁻¹)				
рН	3	n	9	3	n	9
LP	0.0115±0.0001	0.0153±0.0001	0.0144±0.0006	123.6	190.2	190.2
FRSM	0.0815±0.0001	0.0294±0.0006	0.0245±0.0006	380.4	95.1	95.1
CAF	0.0007±0.0001	0.0005±0.0002	0.0008±0.0001	4.1	1.9	3.8
CBZ	0.0027±0.0001	0.0016±0.0001	0.0021±0.0001	7.6	4.7	9.5

n = pH of solution without adjustment (6.0 for LP, 5.5 for FRSM, 5.8 for CAF, 7.1 for CBZ). Errors were calculated from duplicate measurements.

219

Considering the high ε_{254nm} of LP (12 355 M⁻¹ cm⁻¹) at pH 6, its degradation by 220 direct UV-C photolysis could have been supposed. The chemical structure of LP 221 (Table S1) consists of two aromatic rings and various unsaturated bonds and 222 functional groups containing nitrogen, all of which are known as absorbers [11], 223 thus explaining the high molar attenuation coefficient (Table S1) [10]. The 224 225 susceptibility of LP to photolysis at 254 nm in medical formulations based on a drinkable cherry syrup has been reported previously [50, 51]. However, there are 226 no previous reports on the photolysis nor on the values of quantum-yield for LP 227 in water. The quantum yields obtained for LP (Table 1) varied from 0.011 to 0.015 228 mol Einstein⁻¹ (Figure 1, Table 1), and was slightly lower at acidic pH compared 229 to the values obtained at pH 9 and 6 (Figure 1A). The slightly higher molar 230 absorptivity and photolysis coefficients obtained at pH 6 and 9 in comparison to 231

that at pH 3 could be explained by the pKa of this compound (4.15) (Table S1). According to the pKa, LP would exist in its neutral form at pH 3 but in the dissociated form at pH 6 and 9. As the chemical structures of the neutral and the protonated form are distinct, the molar absorptivity may be affected [40]. Specifically, it was slightly higher for the dissociated form of LP than for the neutral form, as confirmed by the ε_{254nm} values which increased from 10 700 M⁻¹ cm⁻¹ at pH 3 to 13 140 M⁻¹ cm⁻¹ at pH 9 (Table S2).

239 As molar attenuation coefficient is influenced by the dissociated/non-dissociated structure and C_p describes a relation between the quantum yield and the molar 240 attenuation coefficient, the C_{ρ} values obtained for LP also varied according to pH 241 (Table 1), specifically being higher at pH 6 and 9 than at pH 3. The C_{ρ} obtained 242 for LP is higher than the value of 40 which indicates that a compound is 243 susceptible to direct photolysis [3]. The C_{ρ} is also similar to those obtained for 244 245 atrazine and pentachlorophenol [4]. Atrazine also presents functional groups that contribute to light absorption and photolysis. Although atrazine exhibits a lower 246 ϵ_{254} (3860 M⁻¹ cm⁻¹ at pH 7) than LP, atrazine has a higher quantum yield (0.046 247 mol Einstein⁻¹). Therefore, these compounds show similar susceptibility to 248 photolysis (C_p atrazine = 160) [4]. In addition to direct UV-C photolysis, chain 249 reactions may be triggered after a compound undergoes photolysis due to the 250 formation of other radicals in the system, such as CI. [4]. Considering that LP, 251 atrazine, and pentachlorophenol all contain chlorine atoms in their structures, Cl-252 radicals may be generated, which would lead to further degradation of these 253 compounds under UV-C irradiation. 254

As shown in Figure S1, FRSM has a lower light absorption coefficient at 254 nm, while it absorbs strongly at 230 nm and 270 nm. In addition, the molar attenuation

coefficients obtained for FRSM at 254 nm ranged from 3200 to 4700 M⁻¹ cm⁻¹, 257 258 corresponding to pH 5.5 and 3, respectively (Table S2). As the pKa of FRSM is 3.9 (Table S1) [52], this compound exists in its neutral form at pH 3, where it 259 exhibited a higher absorptivity and molar attenuation coefficient at 254 nm (Table 260 S2) than at other pH values. As a consequence, photolysis coefficient, and UV-261 C photolysis of FRSM were higher at acidic pH (Table 1, Figure 1). The photo-262 instability of FRSM in the neutral form has been previously reported, and the 263 photolysis product showed increased reactivity, solubility in water, and 264 genotoxicity in comparison to the parent compound [53, 54]. 265

As the molar attenuation coefficient (4660 M⁻¹ cm⁻¹) of FRSM at 254 nm was 266 highest at pH 3, the photolysis coefficient Cp of this compound was more than 3 267 times higher at pH 3 than at pH 5.8 and 9 (Table 1). The photolysis coefficient of 268 FRSM at pH 3 is comparable to that of the antibiotic sulfamethazine, likely due to 269 270 the presence of similar functional groups present, such as sulfonamide and chlorobenzene moieties. These functional groups are light absorbers, thus 271 contributing to UV-C photolysis and to the occurrence of secondary chain 272 reactions [4]. Meanwhile, when the solution pH was above the pKa, the 273 absorbance of the dissociated form of the compound was lower (Table S2). 274 Therefore, molar absorptivity and photolysis coefficients were also lower under 275 these conditions. The quantum yield obtained at pH 5.5 for FRSM was 0.0294 276 mol Einstein⁻¹, which is in agreement with previously reported values (0.02200 \pm 277 0.0028 mol Einstein⁻¹) [55]. 278

The absorption spectrum (Figure S1) of CAF reveals that absorbance of this compound at 254 nm was reduced when compared to 205 nm and 273 nm, and to the absorbance of LP and FRSM at this wavelength. According to the molar

attenuation coefficients obtained at 254 nm (Table S2), the molar absorptivity of 282 283 CAF did not change significantly with pH. This suggests that the structure of CAF is not influenced by the pH, which is in agreement with previous reports that the 284 pKa of CAF is either above 10 [56] or "not observable within the pKa scale in 285 water (0-14)" [10] (Table S1). Therefore, photolysis coefficients obtained for CAF 286 in acidic and basic conditions were similar (Table 1). This testifies for the photo-287 288 stability of CAF over the tested pH range (Figure 1). The quantum yield obtained for CAF in this study was similar to the value reported in the literature (0.0003 289 mol Einstein⁻¹) [12]. Carlson et al. [10] also reported insignificant photolysis of 290 291 caffeine, thus confirming that this compound is not susceptible to UV-C photolysis. As the molar absorptivity was similar at pH 3, 5.5 and 9, the photolysis 292 293 coefficients of CAF were low in all of the tested pH range, ranging from 1.9 to 4.1 294 mol Einstein⁻¹. Interestingly, the photolysis coefficients obtained for CAF were similar to those reported for carbamazepine ($C_p = 7$), which is also resistant to 295 296 UV-C photolysis [4]. As caffeine and carbamazepine have been increasingly detected in water resources, their low susceptibility to photolysis would call for 297 other alternative methods for their treatment in wastewater effluent or in drinking 298 299 water treatment processes.

The absorbance of CBZ at 254 nm was relatively low (Figure S1). Thus, UV-C photolysis of this compound was expected to be relatively low in comparison to compounds that absorb strongly at this wavelength, such as LP. The slightly higher molar attenuation coefficients measured at pH 7 and 9 (Table S2), which are above the pKa (4.2), in comparison to that measured at pH 3, indicate that the substance more readily absorbs photons in its dissociated form. Quantum yield values (Table 1) obtained for CBZ confirm the stability of this compound

under UV-C irradiation (Figure 1). In addition, the quantum yields shown in Table 307 308 1 agree with the values reported previously [57, 58]. The slightly higher decay of CBZ observed at pH 9 in comparison to that at pH 3 or 7 is also in agreement 309 310 with the molar absorptivity values (Table S2). As a consequence of the lower molar attenuation coefficient, the photolysis coefficients of CBZ at different pH 311 are also negligible and comparative to those obtained for CAF. Similarities in the 312 chemical structures (such as the imidazole moiety) of CBZ and CAF may explain 313 the correspondence between the quantum yield and C_p values obtained for both 314 compounds (Table 1, Figures 1C and D). In comparison to other pesticides such 315 316 as atrazine and alachor, CBZ is much more resistant to photolysis [4]. The higher photolysis of atrazine and alachlor in comparison to CBZ may be related to the 317 318 de-chlorination of these compounds [59, 60], which does not occur in CBZ since 319 it does not contain chlorine.

320 3.2 Degradation of target compounds via UV-C/H₂O₂ and UV-C/S₂O₈²⁻

Profiles of the degradation of target compounds, pH values, and consumption of 321 H_2O_2 and $S_2O_8^{2-}$ over the courses of the UV-C AOP are shown in Figure 2. 322 Control experiments consisted of H₂O₂ or S₂O_{8²⁻} in the same concentration 323 without UV-C irradiation, and showed neither removal nor mineralization of target 324 compounds (Figure S2). The use of these oxidants in combination with UV-C 325 326 irradiation increased the removal of all target compounds, especially for the 327 photo-stable compounds CAF and CBZ, resulting in degradation of over 90% (Figure 2) with a dose of 300 to 600 mJ cm⁻² of UV irradiation, depending on the 328 329 target compound.

Figure 2. Left: Degradation of each target compound by UV-C AOPs: UV-C/H₂O₂ and UV-C/S₂O₈²⁻. Control experiments are also presented (UV-C photolysis, H₂O₂, or S₂O₈²⁻ alone). Molar ratio of H₂O₂ or S₂O₈²⁻: compound = 20:1 for LP, FRSM, and CAF, and 32:1 for CBZ; I₀ = 2.41 J m⁻² s⁻¹. Right: consumption (%) of H₂O₂ ($C_0 = 10^{-3}$ M), S₂O₈²⁻ ($C_0 = 10^{-3}$ M), and pH values monitored during UV-C AOPs for each of the target compounds, as functions of incident energy per unit area (mJ cm⁻²).

338

Experiments conducted with LP showed that UV-C photolysis alone achieved up 339 to 85% removal in one hour (corresponding to 870 mJ cm⁻²), while UV-C/S₂O₈²⁻ 340 and UV-C/H₂O₂ reached the same removal rate (Figure 2) after 290 and 620 mJ 341 cm⁻² incident energy, respectively, both achieving 98% removal by 870 mJ cm⁻². 342 UV photolysis of FRSM reached 87% removal after 870 mJ cm⁻² incident energy, 343 while in the presence of H_2O_2 or $S_2O_8^{2-}$, the same efficiency was achieved with 344 345 435 and 650 mJ cm⁻², reaching 98% and 93% removal, respectively, after one hour (Figure 2). Degradation rates of FRSM via UV-C only and UV-C/H₂O₂ 346 determined in this study are in agreement with values reported in the literature 347 [61]. After one hour of reaction (total incident energy 870 mJ cm⁻²), both UV-C 348 AOPs achieved efficient degradation of LP and FRSM, despite the maximum 349 TOC removals being limited to 10% and 6%, respectively (Fig. S2). These results 350 indicate the accumulation of organic transformation products in the system. 351

The limited consumption of H₂O₂ in the presence of LP and FRSM (10%) (Figure 2) probably occurred as a result of the molar attenuation coefficients of these compounds ($\epsilon_{254nm, LP, pH 7}$ =11772 M⁻¹ cm⁻¹, $\epsilon_{254nm, FRSM, pH 6}$ = 3700 M⁻¹ cm⁻¹) (Table S2) being higher than that of H₂O₂ ($\epsilon_{254nm, H2O2}$ = 19.6 M⁻¹ cm⁻¹) [4, 62]. The pharmaceuticals diclofenac and mecoprop, which are strong light absorbers, also impaired the absorption of light by H₂O₂ during UV-C/H₂O₂ treatment [12], thus reducing the process efficiency; this effect is a problem known to occur in the presence of strong photon absorbers [63]. One other reason for the low consumption of H₂O₂ in these systems, when compared to the consumption of S₂O₈²⁻ (25%), may be related to the lower rate constants for the self-scavenging effects of SO₄^{-•} with S₂O₈²⁻ (kso₄-•/s₂O₈₂- = 6:6 x 10⁵ M⁻¹ s⁻¹ and kso₄-•/so₄-• = 3:1 x 10⁸ M⁻¹ s⁻¹) in comparison to those of HO• toward H₂O₂ (koH/H₂O₂= 2:7 x 10⁷ M⁻¹ s⁻¹ and koH•/OH•= 5:5 x 10⁹ M⁻¹ s⁻¹) [17, 64, 65].

As shown in Figure 2 (left column), after 200 mJ cm⁻² of incident energy, the 365 concentrations of LP and FRSM were reduced by a factor of 2. Therefore, 366 competition for light decreased and H₂O₂ and S₂O₈² consumption subsequently 367 increased (Figure 2, right). However, concentrations of both reagents were still 368 369 high at this moment since consumption was lower than 5% of initial concentration (9.5 x 10^{-4} M of remaining H₂O₂ and S₂O₈²⁻) (Figure 2, right column). As 370 regeneration of hydrogen peroxide from hydroxyl radicals via self-scavenging 371 occurs more readily than the regeneration of $S_2O_8^{2-}$ from sulfate radicals, the final 372 consumption of H₂O₂ at the end of treatment was limited to a maximum of 10% 373 of initial concentration after 850 mJ cm⁻² of incident energy, when compared to 374 nearly 30% consumption of $S_2O_8^{2-}$ in the presence of LP and FRSM (Figure 2, 375 376 right column).

During LP degradation, 30% of initial S₂O₈²⁻ were consumed after 430 mJ cm⁻² of incident energy (Figure 2, right column), while H₂O₂ consumption was limited to 10%. Assuming stoichiometric conversion of reagents to oxidative radicals 6 x 10⁻⁴ M of sulfate radicals were generated when compared to 2 x 10⁻⁴ M of hydroxil radicals, thus explaining the faster LP degradation via UV-C/S₂O₈²⁻ (98% within 430 mJ cm⁻²) when compared to the degradation via UV-C/H₂O₂ (70% within 430 mJ cm⁻²) (Figure 2, left). On the other hand, both UV-C AOPs and the UV-C

photolysis exhibited similar patterns in terms of FRSM removal and reagent 384 consumption until 220 mJ cm⁻² of incident energy (Figure 2, left column), 385 suggesting that photolysis was the predominant mechanism in the system, which 386 is supported by the fact that FRSM is a strong light absorber (Section 3.1, Figure 387 1, Table 1). However, after reaching 430 mJ cm⁻² of incident energy, S₂O₈²⁻ 388 consumption reached 21% while only 5% of the initial H₂O₂ had been consumed. 389 Assuming stoichiometric conversions of $S_2O_8^{2-}$ and H_2O_2 to oxidative radicals, 390 nearly 4.2 x 10⁻⁴ M of sulfate radicals were formed in the system, compared to 10⁻¹ 391 ⁴ M of hydroxyl radicals. However, FRSM degradation via UV-C/H₂O₂ at this 392 moment was 99%, while it was only 80% via UV-C/S₂O₈²⁻ (Figure 2, left column). 393 In contrast with LP, for which the degradation was higher in the UV-C/S₂O₈²⁻ 394 system, this result suggests that FRSM is more reactive with hydroxyl radicals 395 396 than with sulfate radicals, which may be related to differences in the chemical 397 structures [3, 15].

CAF and CBZ did not undergo photolysis, which was expected due to their low 398 quantum yields and molar absorption coefficients. In contrast, both UV-C AOPs 399 achieved over 99% removal of CAF and CBZ (Figure 2, left comlumn). CBZ 400 401 degradation was faster via UV-C/H₂O₂, reaching 99% removal after 290 mJ cm⁻² of incident energy, in comparison to the 650 mJ cm⁻² required to achieve similar 402 removal by UV-C/S₂O₈²⁻. Mineralization of CAF and CBZ in the UV-C/S₂O₈²⁻ 403 process was more extensive (reaching 60% and 70%, respectively) than it was 404 in the presence of hydroxyl radicals (reaching 25% and 35%, respectively) 405 (Figure S2). The drop in pH from 9 to 8 during UV-C/S₂O₈²⁻ (which was not 406 observed in UV-C/H₂O₂) was due to the formation of SO_4^{2-} and H⁺ [16]. Higher 407 mineralization rates through UV-C/S $_2O_8^{2-}$ can likely be explained by the greater 408

selectivity and lifespan of sulfate radicals in comparison to hydroxyl radicals as it 409 is less reactive with inorganic species that may be formed during the degradation 410 of target compounds (O, CI-, NO₃⁻ and CO₃²⁻, HCO₃²⁻), and also towards S₂O₈²⁻ and 411 sulfate radical itself (self-scavenging), thus increasing its persistence in the 412 system. This was also reported with other compounds such as 2,4-D, 413 carbamazepine, and azathioprine [14, 66-68]. In addition, the ability UV-C/S₂O₈²⁻ 414 to degrade carboxylic acids and intermediate products usually formed during 415 oxidation processes has been previously confirmed [16]. 416

As CAF and CBZ do not absorb UV-C light as extensively as LP and FRSM, 417 418 irradiation is promptly absorbed by reagents in the UV-C AOPs, leading to higher 419 and faster degradation when compared to UV-C photolysis (Figure 2, Table 2) and higher consumption of H₂O₂ in the UV-C AOPs, reaching 23% for CAF and 420 30% for CBZ (Figure 2). An increase in pH at the beginning of the reactions was 421 observed during UV-C/H₂O₂ treatments of CAF and CBZ (Figure 2 - right 422 column), which likely contributed to higher consumption of H₂O₂ as cleavage is 423 favored in alkaline conditions [69]. S₂O_{8²⁻} consumption exhibited similar behavior 424 to that of H₂O₂ during the degradation of CAF and CBZ. 425

Degradation data obtained during UV-C AOPs were fitted to a pseudo-first-order 426 kinetics model ($R^2 > 0.95$), and apparent rate constants were calculated for each 427 process for the different target compounds (Table 2). Electrical energy per order 428 429 of removal (EE/O; kWh m⁻³) was also calculated in order to compare the efficiencies of the different processes (Table 2). EE/O values represent the 430 amount of energy required to decrease the concentration of the compound by 431 432 one order of magnitude [66]. Therefore, higher k'_{app} values result in lower EE/O values, revealing the most efficient process in terms of lowest energy 433

consumption [70]. However, EE/O should not be considered alone when aiming 434 435 to identify the most affordable process; reagent costs must also be considered, as, for example, persulfate is more expensive than H₂O₂ [71]. When compared to 436 UV-C photolysis alone, k'app values increased in the presence of hydroxyl and 437 sulfate radicals. Regarding UV-C photolysis, the EE/O values (Table 2) were 438 calculated using experimental data for FRSM, as this process reduced the 439 concentration of this compound by one order of magnitude within 650 mJ cm⁻² of 440 incident energy. In contrast, for LP, EE/O values were predicted using the k'UV-C 441 obtained for this compound. As UV-C photolysis of CAF and CBZ did not fit the 442 pseudo-first-order model ($R^2 < 0.95$), it was not possible to estimate EE/O values 443 for the photolysis of these compounds. Apparent rate constants values for the 444 degradation of CAF via UV-C/H₂O₂ agree with the values obtained by Shu et al. 445 446 [12], who reported higher values of these constants for compounds with reduced quantum yields (caffeine and carbamazepine). Therefore, data on the photolysis 447 448 coefficients and quantum yields of emerging contaminants present in water may 449 be a valuable tool to predict their degradability via UV-C photolysis, or whether UV-C AOPs would need to be applied [3]. 450

451 Apparent rate constants obtained for the UV-C/H₂O₂ process were higher than those of the UV-C/S₂O_{8²⁻} process for all target compounds except LP. This is 452 likely due to the higher reaction rate of this compound with sulfate radical than 453 with the hydroxyl radical. A decrease in the concentration of LP by one order of 454 magnitude occurred after 20 minutes (290 mJ cm⁻² of incident energy) for UV-455 $C/S_2O_8^{2-}$ (Figure 2), yet 45 minutes (650 mJ cm⁻²) were required to achieve the 456 same removal (Table 2) by UV-C/H₂O₂, as reflected in the k'_{app} and EE/O values. 457 The lower k'_{app} values obtained for UV-C/S₂O₈²⁻ compared to that of UV-C/H₂O₂ 458

459	during the degradation of FRSM, CAF, and CBZ may be related to the higher
460	selectivity of SO4-• when compared to that of HO•, since it acts preferentially via
461	electron transfer whereas HO• also reacts via addition and H-abstraction [72].
462	UV-C/H ₂ O ₂ required 20 minutes (290 mJ cm ⁻²) to reduce the FRSM concentration
463	by one order of magnitude, while 45 minutes (650 mJ cm ⁻²) were required by UV-
464	$C/S_2O_8^{2-}$, thus explaining the higher EE/O of the former process (Table 2).

Table 2 – Pseudo-first-order rate constants (min⁻¹) obtained for each process for the different target compounds, and EE/O values obtained for UV-C/H₂O₂ and UV-C/S₂O₈²⁻ for the different target compounds

Pseudo-first-order rate constant (k'; min ⁻¹)	LP	FRSM	CAF	CBZ	
k' _{UV-C}	0.011±0.005	0.056±0.004	*	*	
<i>k'</i> υv-с/н202	0.048±0.0003	0.11±0.01	0.100±0.001	0.22±0.01	
K'UV-C/S2O82-	0.0864±0.0005	0.072±0.002	0.085±0.007	0.17±0.04	
EE/O (kWh m ⁻³)					
UV-C	2.3 P**	1.5 P			
UV-C/H ₂ O ₂	1.5 P	0.67 P	0.5 P	0.25 P	
UV-C/S2O8 ²⁻	0.6 P	1.5 P	0.5 P	0.33 P	

*Did not fit the model due to low degradation ($R^2 < 0.95$). P is the lamp power (10 W) **Estimated using the k'_{UV-C} value.

468

469 The EE/O values obtained for CAF degradation were the same for both UV-C AOPs (0.5 P), indicating that the energy required to remove this compound in 470 water using either H₂O₂ or S₂O_{8²⁻} under UV-C irradiation was the same. This 471 result agrees with the similarity between the kinetic rates obtained for each 472 process (Table 2). For CBZ, both UV-C AOPs showed comparable k'app and EE/O 473 474 values (Table 2). The degradation of carbamazepine, another photo-resistant compound, via UV-C/H₂O₂ and UV-C/S₂O₈²⁻ also led to similar EE/O values in a 475 previous study [22]. Indeed, the quantum yield, photolysis coefficient, molar 476 mass, and chemical composition of CAF and CBZ are all very similar, which might 477 explain their comparable behavior when submitted to UV-C AOPs. 478

479 3.4 Evolution of acute toxicity

As shown in Figure 3, acute toxicity varied between treatments for all compounds, 480 indicating the formation of toxic intermediates during UV-C AOPS, as has been 481 reported in the literature for various emerging contaminants [23]. The LP solution 482 was not toxic to Allivibrio fischeri (a.T.u. = 0.26), and no acute toxicity was 483 observed during UV-C/H₂O₂ treatment. However, acute toxicity developed during 484 the UV-C-only and UV-C/S₂O₈²⁻ processes, despite the high degradation 485 efficiencies achieved during these processes (65% for UV-C and 98% for UV-486 $C/S_2O_{8^2}$). According to Adachi et al. [73], the cyanide ion is formed when LP is 487 oxidized by sodium hypochlorite. Therefore, this ion could have been formed by 488 oxidation during the UV-C AOPs, which may have contributed to the increase in 489 acute toxicity. This difference between the degradation by sulfate and by hydroxyl 490 radicals have been described in previous studies [24]. However, there is no report 491 492 in the literature regarding the formation of toxic transformation products during UV-C photolysis and UV-C/S₂O₈²⁻ oxidation of LP, nor of other sartans with similar 493 structures. In contrast, the EE/O values suggest that UV-C/S₂O₈²⁻ is more efficient 494 than UV-C/H₂O₂ in the removal of LP. This result indicates that it is not adequate 495 to consider the EE/O values alone for identifying the optimal treatment method. 496

497

Figure 3. Acute toxicity of samples withdrawn during the degradation of target compounds via UV-C, UV-C/H₂O₂, and UV-C/S₂O₈²⁻ processes, shown as functions of the total incident energy received (mJ cm⁻²). The horizontal lines represent the threshold of 1.21 a.T.u.; bars crossing the line thus indicate toxic samples.

503

504 FRSM was reported to be non-toxic to Allivibrio fischeri [54], yet its products of

505 photolysis and electro-Fenton degradation are considered toxic [74, 75]. In the 506 present study, before treatment, the FRSM solution exhibited a beneficial stimulatory effect, known as hormesis, upon the photobacteria (Figure 3). This 507 508 effect occurs with luminescent bacteria as a consequence of exposure to small concentrations of toxic chemicals [76]. As shown in Figure 3, acute toxicity was 509 generated during the UV-C photolysis of FRSM, but was eliminated within 600 510 mJ cm⁻² of incident energy, when this process reached FRSM removal of 80% 511 (Figure 2). Meanwhile, there was no generation of toxicity during the UV-C/H₂O₂ 512 process. In contrast, UV-C/S₂O₈²⁻ exhibited similar behavior to the UV-C-only 513 514 process, as toxicity was generated at the beginning of the reaction but was eliminated within 300 mJ cm⁻² of incident energy, much less than that required 515 with the UV-C-only process (Figure 3). 516

Before treatment, the CAF solution exhibited an inhibitory effect ($Ec_{50} = 76\%$; 517 518 a.T.u. = 1.3) on Allivibrio fischeri, as has been reported for similar tests using a marine photobacterium as a bioindicator (Ec50 = 62.8%) [77]. Although a few 519 authors reported that there was no increase in CAF toxicity after AOP treatments 520 [78, 79], no reports on the effect of UV-C/H₂O₂ or UV-C/S₂O_{8²⁻} on CAF toxicity 521 have been published. This is alarming since caffeine is detected in surface waters 522 in a wide variety of locations in concentrations up to $\mu g L^{-1}$ [34], and was even 523 considered for use as an indicator of illegal sewage disposal [37]. Both UV-524 C/H_2O_2 and $UV-C/S_2O_8^{2-}$ increased CAF toxicity at the beginning of the treatment, 525 526 although the toxic effects were entirely eliminated toward the end of the treatments when the concentration of CAF was below 10% of its initial 527 concentration (Figure 3). This suggests the formation and degradation of toxic 528 529 transformation products within both processes. With regards to UV-C photolysis,

for which only the final sample was analyzed due to the negligible effect of this
process on the removal of CAF, an increase in toxicity during treatment was also
observed.

As confirmed by the results shown in Figure 3, CBZ is known to be toxic to 533 Allivibrio fischeri [80]. Similarly to what was observed for CAF, UV-C photolysis 534 alone was not able to remove CBZ due to its low molar absorptivity and quantum 535 yield. Consequently, UV-C photolysis had a negligible effect on the acute toxicity 536 of CBZ. Meanwhile, both UV-C/H₂O₂ and UV-C/S₂O₈²⁻ eliminated the toxic effect 537 of CBZ; as it was also observed by other irradiated AOPs under artificial and solar 538 irradiation in another study [80]. During UV-C/H₂O₂, CBZ degradation occurred 539 alongside the reduction in acute toxicity (Figure 3). In contrast, acute toxicity 540 increased during the initial stages of the UV-C/S₂O₈²⁻ process and decreased 541 toward the end, probably due to the formation of toxic transformation products. 542 543 This result agrees with the EE/O values (Table 2), as less energy was required to reduce the toxicity of CBZ via UV-C/H₂O₂ compared to UV-C/S₂O₈²⁻. 544

3.5 Degradation of target compounds by UV-C/H₂O₂ and UV-C/S₂O₈²⁻ in surface
water

In order to assess the impact of the water matrix on the degradation of target compounds, UV-C, UV-C/H₂O₂, and UV-C/ S₂O₈²⁻ treatments were applied to surface water and ultrapure water each spiked with 10 μ M of each compound. Although degradation of all compounds occurred simultaneously, since all compounds were present in the same matrix, the degradation of each pollutant was quantified individually (Figure 3). Reduction in TOC and consumption of H₂O₂ and S₂O₈²⁻ were also monitored (Figure 4).

554

Figure 4. Degradation of LP, FRSM, CAF, and CBZ (10 μ M each) in ultra-pure water and surface water by UV-C, UV-C/H₂O₂, and UV-C/S₂O_{8²⁻} processes (*C*_{0H2O2 or S2O82-} = 10⁻³ M), shown as functions of total incident energy per area (mJ cm⁻²).

The presence of scavenger compounds that are naturally present in real surface 560 561 water, including HCO₃, natural organic matter (NOM), and Cl, among others, may lead to a lower degradation of target compounds in practical applications 562 563 [70]. NOM is mainly comprised of humic acids which present various functional groups that compete with the target compounds for hydroxyl and sulfate radicals 564 [81, 82]. As shown in Figure 4, UV-C photolysis of CBZ in the surface water and 565 566 in the presence of the other target compounds was similar to that observed in pure water, still exhibiting an insignificant decrease in concentration due to its 567 lower quantum yield and molar absorptivity at 254 nm (Table 1). On the other 568 hand, the UV-C photolysis of each of LP, FRSM, and CAF was slightly higher in 569 surface water than in pure water. This likely happened due the formation of 570 oxidative radicals from the natural constituents of the Lys River surface water, 571 which presented a DOC of 1.2 mg L⁻¹; O₂ concentration 8 mg L⁻¹; NO₃⁻ 572 concentration 22 mg L⁻¹; PO₄³⁻ concentration 0.1 mg L⁻¹; Cl⁻ concentration 20 mg 573 574 L⁻¹; and high alkalinity of 330 mg L⁻¹ HCO₃. A greater extent of photolysis of 575 FRSM in natural waters than in pure water was also observed previously [61]. When NOM, dissolved oxygen, and phosphate are submitted to UV-C_{254nm} 576 577 irradiation, oxidative species such as NOM \bullet , singlet oxygen (${}^{1}O_{2}$), and PO $_{4}{}^{2}\bullet$ may be formed [83, 84]. Although these radicals present lower redox potentials than 578 579 HO• and SO₄••, they may have contributed to the enhanced photolysis of LP, FRSM, and CAF [85]. Further, HO• may also be formed from the irradiation of 580

581 NO_3^- present in surface waters [86, 87].

Lower degradations of LP and FRSM were observed during UV-C AOPs in 582 surface water than in pure water. The high level of carbonate ions in surface water 583 may have contributed to the guenching of hydroxyl and sulfate radicals involved 584 in the degradation reactions. In contrast, for CAF and CBZ, the effect of matrix 585 constituents on the oxidative radicals formed during the UV-C AOPs could not be 586 observed, probably because their reaction rates with radicals are extremely high, 587 as shown in Table 2. The relatively high content of chloride ions, which react 588 strongly with sulfate radicals [88], may have influenced the effectiveness of the 589 $UV-C/S_2O_8^{2-}$ process, thus leading to the lower removal of target compounds in 590 surface water than in pure water. 591

The consumption rates of H_2O_2 and $S_2O_8^{2-}$ were below 25% in all of the tested 592 conditions (Figure 5). H₂O₂ consumption in pure water was 13%, but 20% in 593 surface water, thus confirming that a higher consumption of this reagent occurred 594 in the presence of other matrix components. On the other hand, S₂O₈²⁻ 595 consumption was very similar in pure water (20%) and in the presence of matrix 596 597 components (24%). In addition, previous studies have confirmed that the performance of the UV-C/S₂O₈²⁻ process is not disturbed by carbonate ions 598 599 (HCO_3) to such an extent as is the performance of the UV-C/H₂O₂ process, probably due to the lower reaction constants for the reaction of SO4-• with HCO3-600 $(k_{SO4^{\bullet}}, HCO3 = 2.8 \times 10^{6} \text{ M}^{-1} \text{ s}^{-1})$ than that of OH• with HCO3⁻ $(k_{HO}^{\bullet}, HCO3 = 8.5 \times 10^{6} \text{ s}^{-1})$ 601 M⁻¹ s⁻¹) [6, 14, 17-19]. Furthermore, the TOC removal (Figure 5) achieved by UV-602 603 $C/S_2O_8^{2-}$ (9% and 21% in pure water and surface water, respectively) was higher than that achieved by UV-C/H₂O₂ (5.7 and 14.9%, respectively) in both water 604 605 matrices, thus corroborating the results reported earlier in this study (Section 3.3).

The higher mineralization efficiency in surface water than in pure water corresponds to the degradation of NOM via sulfate radicals, as reported previously [65].

609

Figure 5. Reagent consumption and TOC removal during UV-C AOPs in surface water (filled symbols) and pure water (empty symbols), as functions of total incident energy per area (mJ cm⁻²) (Initial TOC in pure water 5.4 mg L⁻¹ and in surface water 6.6 mg L⁻¹).

614

615 3.3 Identification of transformation products

616 The mass spectra of CAF before UV-C radiation (zero min) shows two peaks: protonated caffeine I ([caffeine+H⁺], m/z = 195.08) and another signal 617 ([caffeine+Na⁺], m/z = 217.07) which refers to the sodium adduct (Figure 6A). The 618 peak intensities corresponding to the transformation products detected during 619 CAF oxidation, along with the mass spectra after 315 mJ cm⁻² of incident energy 620 621 in the UV-C/H₂O₂ (Figures 6B and C) and UV-C/S₂O_{8²⁻} (Figures 6D and E) 622 processes show that a higher number of transformation products were formed during UV-C/H₂O₂ than during UV-C/S₂O_{8²⁻, likely due to the higher selectivity of} 623 624 the sulfate radical than the hydroxyl radical. The oxidation of the six-membered ring in UV-C/H₂O₂ first generated 2 main species which presented masses m/z =625 125.98 and 142.06 (Figures 6B and C, at 50 mJ cm⁻², and Figure 7), with smaller 626 peaks corresponding to *m*/*z* 128.02 and 168.04 (Figures 6B and C and Figure 7). 627 However, after 300 mJ cm⁻² of incident energy, species with m/z = 110.01, 628 128.02, and 146.03 were identified in the UV-C/H₂O₂ system (Figures 6B and C 629 and Figure 7). 630

Figure 6. Mass spectra of (A) Caffeine solution in pure water, (B and D) signals corresponding to masses detected during UV-C/H₂O₂ and UV-C/S₂O₈²⁻ treatments, and (C and E) mass spectra obtained after UV-C/H₂O₂ and UV- $C/S_2O_8^{2-}$ treatments with 300 mJ cm⁻² of total incident energy.

Meanwhile, the transformation products accumulated during UV-C/ $S_2O_8^{2-}$ were different (m/z = 164.92 and 142.94; Figures 6D and E), thus suggesting a different transformation pathway which has not yet been reported for caffeine in the literature. These results are very relevant considering that the use of caffeine as an indicator of so-called 'fresh' contamination of surface waters has been suggested by some authors [35-37].

Considering the spectra obtained during the degradation of CAF via UV-C/H₂O₂, 642 a possible degradation route was proposed, as shown in Figure 7. The signal at 643 644 m/z = 195.09 (structure I) corresponds to the protonated adduct of caffeine. The oxidation process led to a decrease in intensity of the m/z = 195 signal and 645 increases in the intensities of other signals associated to products of oxidation. 646 ChemCalc [89] was used to assign a formula to the exact mass and then propose 647 a structure based on these formulae. The two first products (II: m/z = 142.06 and 648 649 III: m/z = 125.98) would be formed from a break of the pyrimidine moiety and the opening of the imidazole ring (Figure 7). A signal of m/z 142 was also detected 650 651 by Dalmazio et al., (2005) [90] during the degradation of caffeine via UV-C/H₂O₂. 652 However, considering the exact mass obtained here, the product proposed in the 653 referred paper was not realistic in our case. Species of m/z 128.02 (III) and 146.03 (IV) would be formed from the further oxidation of II, leading to an 654 655 isocyanate structure [80] and the formation of carboxylic acid moieties. Then, 656 compound VI would later accumulate in the system as a product of oxidation of the intermediate compounds. However, no structure could be proposed for the 657

detected signals. No structures were proposed for the oxidation products of the $UV/S_2O_8^{2-}$ process, as the formulae proposed for the mass obtained were not relevant for the process [89].

Figure 7. Degradation pathway proposed for the formation of transformation
 products generated during the oxidation of caffeine via UV-C/H₂O₂

663

These analyses were also performed with samples withdrawn during the oxidation of LP, FRSM, and CBZ via UV-C/H₂O₂ and UV-C/S₂O₈²⁻. However, as shown in Figures S3, S4, and S5, decreases in the signal intensities of the target compounds were observed, yet no other signals of significant intensity were detected. TPs could not be observed using this methodology as they would not have been ionized by the ESI used here.

670 4. Conclusion

In this study, the quantum yields and photolysis coefficients were calculated for 671 target compounds, indicating that LP and FRSM are susceptible to photolysis in 672 the UV-C range (80% removal of each LP and FRSM under UV-C photolysis 673 alone at total levels of 800 and 600 mJ cm⁻² incident energy). In contrast, the UV-674 C photolysis of both CAF and CBZ by this process was negligible. UV-C/H₂O₂ 675 and UV-C/S₂O_{8²⁻ were extremely effective in the removal of all target compounds,} 676 achieving over 90% degradation in a pure water matrix under the same 677 conditions. k'app rates were obtained for UV-C/H2O2 on the degradation of FRSM, 678 CAF, and CBZ, when compared to UV-C/ $S_2O_8^{2-}$ due to the reactivity of hydroxyl 679 680 radicals toward these compounds and their intermediates. On the other hand, mineralization rates and reagent consumption were higher in the UV-C/S₂O₈²⁻ 681 682 system, probably due to the greater light absorption and lower self-scavenging

exhibited by sulfate radicals as compared to hydroxyl radicals. During acute 683 toxicity analysis using Allivibrio fischeri, samples withdrawn during the UV-C-only 684 and UV-C/S₂O₈²⁻ processes exhibited higher toxicity than those withdrawn during 685 the UV-C/H₂O₂ process. Simultaneous degradation of target compounds in real 686 surface water indicated higher stability of the UV-C/S₂O₈²⁻ system in the presence 687 of natural scavengers in comparison to that of the UV-C/H₂O₂ system. A lower 688 number of transformation products were detected during CAF degradation via 689 UV-C/S₂O₈²⁻ as compared to UV-C/H₂O₂, confirming the higher selectivity of the 690 sulfate radical than the hydroxyl radical, and suggesting distinct reaction 691 mechanisms for each radical. 692

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699 References

- [2] E.A. Serna-Galvis, F. Ferraro, J. Silva-Agredo, R.A. Torres-Palma, Degradation of highly
 consumed fluoroquinolones, penicillins and cephalosporins in distilled water and simulated
 hospital wastewater by UV254 and UV254/persulfate processes, Water Research 122 (2017)
 128-138.
- [3] D. Gerrity, Y. Lee, S. Gamage, M. Lee, A.N. Pisarenko, R.A. Trenholm, U. von Gunten, S.A.
 Snyder, Emerging investigators series: prediction of trace organic contaminant abatement with

710 UV/H2O2: development and validation of semi-empirical models for municipal wastewater

effluents, Environmental Science: Water Research & Technology 2 (2016) 460-473.

 ^[1] S. Giannakis, M. Voumard, D. Grandjean, A. Magnet, L.F. De Alencastro, C. Pulgarin,
 Micropollutant degradation, bacterial inactivation and regrowth risk in wastewater effluents:
 Influence of the secondary (pre)treatment on the efficiency of Advanced Oxidation Processes,
 Water Research 102 (2016) 505-515.

- 712 [4] D.R. Hokanson, K. Li, R.R. Trussell, A photolysis coefficient for characterizing the response of
- aqueous constituents to photolysis, Frontiers of Environmental Science & Engineering 10 (2016)
 428-437.
- [5] J.C. Kruithof, P.C. Kamp, B.J. Martijn, UV/H2O2 Treatment: A Practical Solution for Organic
 Contaminant Control and Primary Disinfection, Ozone: Science & Engineering 29 (2007) 273-
- 717 280.
- 718 [6] C. Luo, J. Ma, J. Jiang, Y. Liu, Y. Song, Y. Yang, Y. Guan, D. Wu, Simulation and comparative
- study on the oxidation kinetics of atrazine by UV/H2O2, UV/HSO5- and UV/S2O82-, Water
 Research 80 (2015) 99-108.
- 721 [7] M.A. Tarr, Chemical Degradation Methods for Wastes and Pollutantes, New York, 2003.
- [8] G. Boczkaj, A. Fernandes, Wastewater treatment by means of advanced oxidation processes
 at basic pH conditions: A review, Chemical Engineering Journal 320 (2017) 608-633.
- [9] M.A. Oturan, J.-J. Aaron, Advanced Oxidation Processes in Water/Wastewater Treatment:
 Principles and Applications. A Review, Critical Reviews in Environmental Science and Technology
 44 (2014) 2577-2641.
- [10] J.C. Carlson, M.I. Stefan, J.M. Parnis, C.D. Metcalfe, Direct UV photolysis of selected
 pharmaceuticals, personal care products and endocrine disruptors in aqueous solution, Water
- 729 Research 84 (2015) 350-361.
- [11] R.F. Dantas, O. Rossiter, A.K.R. Teixeira, A.S.M. Simões, V.L. da Silva, Direct UV photolysis of
 propranolol and metronidazole in aqueous solution, Chemical Engineering Journal 158 (2010)
 143-147.
- [12] Z. Shu, J.R. Bolton, M. Belosevic, M. Gamal El Din, Photodegradation of emerging
 micropollutants using the medium-pressure UV/H2O2 Advanced Oxidation Process, Water
 Research 47 (2013) 2881-2889.
- [13] M. Muruganandham, R.P.S. Suri, S. Jafari, Sillanp, #xe4, M., G.-J. Lee, J.J. Wu, M.
 Swaminathan, Recent Developments in Homogeneous Advanced Oxidation Processes for Water
 and Wastewater Treatment, International Journal of Photoenergy 2014 (2014) 21.
- [14] Y. Zhang, J. Zhang, Y. Xiao, V.W.C. Chang, T.-T. Lim, Kinetic and mechanistic investigation of
 azathioprine degradation in water by UV, UV/H2O2 and UV/persulfate, Chemical Engineering
 Journal 302 (2016) 526-534.
- [15] M.-S. Tsao, W.K. Wilmarth, The Aqueous Chemistry of Inorganic Free Radicals. I. The
 Mechanism of the Photolytic Decomposition of Aqueous Persulfate Ion and Evidence Regarding
 the Sulfate–Hydroxyl Radical Interconversion Equilibrium, The Journal of Physical Chemistry 63
 (1959) 346-353.
- 746 [16] J. Criquet, N.K.V. Leitner, Degradation of acetic acid with sulfate radical generated by747 persulfate ions photolysis, Chemosphere 77 (2009) 194-200.
- 748 [17] G.V. Buxton, C.L. Greenstock, W.P. Helman, A.B. Ross, Critical Review of rate constants for 749 reactions of hydrated electrons, hydrogen atoms and hydroxyl radicals (·OH/·O– in Aqueous
- Solution, Journal of Physical and Chemical Reference Data 17 (1988) 513-886.
 [18] O.P. Chawla, R.W. Fessenden, Electron spin resonance and pulse radiolysis studies of some
- reactions of peroxysulfate (SO4.1,2), The Journal of Physical Chemistry 79 (1975) 2693-2700.
- 753 [19] M.G. Antoniou, H.R. Andersen, Comparison of UVC/S2O82- with UVC/H2O2 in terms of
- efficiency and cost for the removal of micropollutants from groundwater, Chemosphere 119(2015) S81-S88.
- 756 [20] S. Wacławek, H.V. Lutze, K. Grübel, V.V.T. Padil, M. Černík, D.D. Dionysiou, Chemistry of 757 persulfates in water and wastewater treatment: A review, Chemical Engineering Journal 330
- 758 (2017) 44-62.
- 759 [21] Y. Yang, J.J. Pignatello, J. Ma, W.A. Mitch, Effect of matrix components on UV/H2O2 and
- 760 UV/S2O82– advanced oxidation processes for trace organic degradation in reverse osmosis
- 761 brines from municipal wastewater reuse facilities, Water Research 89 (2016) 192-200.

- [22] L. Lian, B. Yao, S. Hou, J. Fang, S. Yan, W. Song, Kinetic Study of Hydroxyl and Sulfate RadicalMediated Oxidation of Pharmaceuticals in Wastewater Effluents, Environmental Science &
 Technology 51 (2017) 2954-2962.
- [23] A. Sharma, J. Ahmad, S.J.S. Flora, Application of advanced oxidation processes and toxicity
 assessment of transformation products, Environmental Research 167 (2018) 223-233.

767 [24] Y. Yang, X. Lu, J. Jiang, J. Ma, G. Liu, Y. Cao, W. Liu, J. Li, S. Pang, X. Kong, C. Luo, Degradation
768 of sulfamethoxazole by UV, UV/H2O2 and UV/persulfate (PDS): Formation of oxidation products
769 and effect of bicarbonate, Water Research 118 (2017) 196-207.

- [25] K. Yin, L. Deng, J. Luo, J. Crittenden, C. Liu, Y. Wei, L. Wang, Destruction of phenicol
 antibiotics using the UV/H2O2 process: Kinetics, byproducts, toxicity evaluation and
 trichloromethane formation potential, Chemical Engineering Journal 351 (2018) 867-877.
- [26] T. Olmez-Hanci, I. Arslan-Alaton, D. Dursun, B. Genc, D.G. Mita, M. Guida, L. Mita,
 Degradation and toxicity assessment of the nonionic surfactant Triton[™] X-45 by the
 peroxymonosulfate/UV-C process, Photochemical & Photobiological Sciences 14 (2015) 569575.
- 777 [27] Q. Zhang, J. Chen, C. Dai, Y. Zhang, X. Zhou, Degradation of carbamazepine and toxicity
- evaluation using the UV/persulfate process in aqueous solution, Journal of Chemical Technology& Biotechnology 90 (2015) 701-708.
- [28] E.S. Gonçalves, OCORRÊNCIA E DISTRIBUIÇÃO DE FÁRMACOS, CAFEÍNA E BISFENOL-A EM
 ALGUNS CORPOS HÍDRICOS NO ESTADO DO RIO DE JANEIRO, Departamento de Geociências da
 Universidade Federal Fluminense, Universidade Federal Fluminense, Niterói, RJ, 2012, pp. 197.
- 783 [29] T. Heberer, Tracking persistent pharmaceutical residues from municipal sewage to drinking
 784 water, Journal of Hydrology 266 (2002) 175-189.
- [30] D.G.J. Larsson, C. de Pedro, N. Paxeus, Effluent from drug manufactures contains extremely
 high levels of pharmaceuticals, Journal of Hazardous Materials 148 (2007) 751-755.
- [31] C.D.S. Pereira, L.A. Maranho, F.S. Cortez, F.H. Pusceddu, A.R. Santos, D.A. Ribeiro, A. Cesar,
 L.L. Guimarães, Occurrence of pharmaceuticals and cocaine in a Brazilian coastal zone, Science
 of The Total Environment 548 (2016) 148-154.
- [32] M.A. Sousa, C. Gonçalves, V.J.P. Vilar, R.A.R. Boaventura, M.F. Alpendurada, Suspended
 TiO2-assisted photocatalytic degradation of emerging contaminants in a municipal WWTP
 effluent using a solar pilot plant with CPCs, Chemical Engineering Journal 198 (2012) 301-309.
- [33] F. Stuer-Lauridsen, M. Birkved, L.P. Hansen, H.C. Holten Lützhøft, B. Halling-Sørensen,
 Environmental risk assessment of human pharmaceuticals in Denmark after normal therapeutic
 use, Chemosphere 40 (2000) 783-793.
- [34] M.C.V.M. Starling, C.C. Amorim, M.M.D. Leão, Occurrence, control and fate of contaminants
 of emerging concern in environmental compartments in Brazil, Journal of Hazardous Materials
 (2018).
- [35] S. Froehner, W. Piccioni, K.S. Machado, M.M. Aisse, Removal Capacity of Caffeine,
 Hormones, and Bisphenol by Aerobic and Anaerobic Sewage Treatment, Water, Air, & Soil
 Pollution 216 (2011) 463-471.
- [36] C.C. Montagner, W.F. Jardim, P.C. Von der Ohe, G.A. Umbuzeiro, Occurrence and potential
 risk of triclosan in freshwaters of São Paulo, Brazil—the need for regulatory actions,
 Environmental Science and Pollution Research 21 (2014) 1850-1858.
- [37] F.F. Sodré, M.A.F. Locatelli, W.F. Jardim, Occurrence of Emerging Contaminants in Brazilian
 Drinking Waters: A Sewage-To-Tap Issue, Water, Air, and Soil Pollution 206 (2010) 57-67.
- [38] M.K. Burkhardt, T.; Hean, S.; Schmid, P.; Haag, R.; Rossi, L.; Boller, M., Release of biocides
 from urban areas into aquatic systems, 6th International conference on sustainable techniques
 and strategies in urban water management (NOVATECH)Lyon, France, 2007.
- 810 [39] M. Loewy, V. Kirs, G. Carvajal, A. Venturino, A.M. Pechen de D'Angelo, Groundwater
- 811 contamination by azinphos methyl in the Northern Patagonic Region (Argentina), Science of The
- 812 Total Environment 225 (1999) 211-218.

- [40] S. Canonica, L. Meunier, U. von Gunten, Phototransformation of selected pharmaceuticals
 during UV treatment of drinking water, Water Research 42 (2008) 121-128.
- 815 [41] I. Nicole, J. De Laat, M. Dore, J.P. Duguet, C. Bonnel, Utilisation du rayonnement ultraviolet
- dans le traitement des eaux: mesure du flux photonique par actinometrie chimique au peroxyde
 d'hydrogene, Water Research 24 (1990) 157-168.

[42] J.F.F. ANDERSON, M.C.G. GERLIN, R.A. SVERSUT, L.C.S. OLIVEIRA, A.K. SINGH, M.S. AMARAL,
N.M. KASSAB, Development and Validation of an Isocratic HPLC Method for Simultaneous
Determination of Quaternary Mixtures of Antihypertensive Drugs in Pharmaceutical
Formulations Acta Chromatographica 29(2017) (2016) 95–110.

- [43] EPA, Method 631: The Determination of Benomyl and Carbendazim in Municipal and Industrial Wastewater in: EPA (Ed.), EPA, 1993.
- [44] EPA, Method 1694: Pharmaceuticals and Personal Care Products in Water, Soil, Sediment,
 and Biosolids by HPLC/MS/MS EPA, 2007.
- [45] F.J. Beltran, G. Ovejero, J.F. Garcia-Araya, J. Rivas, Oxidation of Polynuclear Aromatic
 Hydrocarbons in Water. 2. UV Radiation and Ozonation in the Presence of UV Radiation,
 Industrial & Engineering Chemistry Research 34 (1995) 1607-1615.
- [46] V.M. Amin, N.F. Olson, Spectrophotometric Determination of Hydrogen Peroxide in Milk1,
 Journal of Dairy Science 50 (1967) 461-464.
- [47] M.C.V.M. Starling, L.A.S. Castro, R.B.P. Marcelino, M.M.D. Leão, C.C. Amorim, Optimized
 treatment conditions for textile wastewater reuse using photocatalytic processes under UV and
 visible light sources, Environmental Science and Pollution Research 24 (2017) 6222-6232.
- [48] A.J. Poole, Treatment of biorefractory organic compounds in wool scour effluent by
 hydroxyl radical oxidation, Water Research 38 (2004) 3458-3464.
- [49] T. Olmez-Hanci, I. Arslan-Alaton, D. Dursun, Investigation of the toxicity of common oxidants
 used in advanced oxidation processes and their quenching agents, Journal of Hazardous
 Materials 278 (2014) 330-335.
- [50] S. Kollipara, G. Bende, Y. Bansal, R. Saha, Stability-indicating Reversed-phase Liquid
 Chromatographic Method for Simultaneous Determination of Losartan Potassium and Ramipril
 in Tablets, Indian Journal of Pharmaceutical Sciences 74 (2012) 201-210.
- [51] R.A. Seburg, J.M. Ballard, T.-L. Hwang, C.M. Sullivan, Photosensitized degradation of
 losartan potassium in an extemporaneous suspension formulation, Journal of Pharmaceutical
 and Biomedical Analysis 42 (2006) 411-422.
- 845 [52] S.J. Khan, J.E. Ongerth, Modelling of pharmaceutical residues in Australian sewage by 846 quantities of use and fugacity calculations, Chemosphere 54 (2004) 355-367.
- 847 [53] D.E. Moore, C.D. Burt, PHOTOSENSITIZATION BY DRUGS IN SURFACTANT SOLUTIONS,
 848 Photochemistry and Photobiology 34 (1981) 431-439.
- [54] M. Isidori, A. Nardelli, A. Parrella, L. Pascarella, L. Previtera, A multispecies study to assess
 the toxic and genotoxic effect of pharmaceuticals: Furosemide and its photoproduct,
 Chemosphere 63 (2006) 785-793.
- 852 [55] B.A. Wols, D.J.H. Harmsen, E.F. Beerendonk, C.H.M. Hofman-Caris, Predicting
 853 pharmaceutical degradation by UV (LP)/H2O2 processes: A kinetic model, Chemical Engineering
 854 Journal 255 (2014) 334-343.
- [56] D.W. Newton, R.B. Kluza, pKa Values of Medicinal Compounds in Pharmacy Practice, Drug
 Intelligence & Clinical Pharmacy 12 (1978) 546-554.
- [57] R. Panadés, A. Ibarz, S. Esplugas, Photodecomposition of carbendazim in aqueous solutions,
 Water Research 34 (2000) 2951-2954.
- [58] P. Mazellier, É. Leroy, B. Legube, Photochemical behavior of the fungicide carbendazim in
 dilute aqueous solution, Journal of Photochemistry and Photobiology A: Chemistry 153 (2002)
 221-227.
- 862 [59] Y. Souissi, S. Bouchonnet, S. Bourcier, K.O. Kusk, M. Sablier, H.R. Andersen, Identification
- 863 and ecotoxicity of degradation products of chloroacetamide herbicides from UV-treatment of
- 864 water, Science of The Total Environment 458-460 (2013) 527-534.

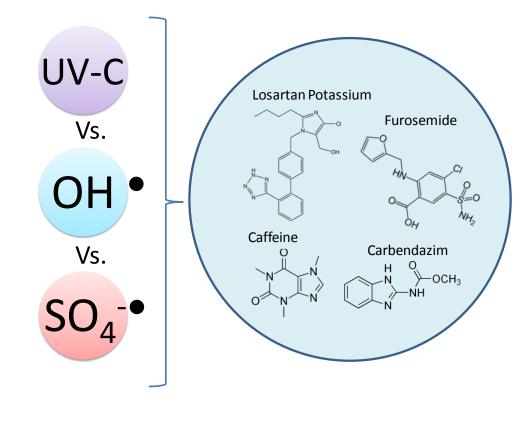
- [60] H.-J. Choi, D. Kim, T.-J. Lee, Photochemical degradation of atrazine in UV and UV/H2O2
 process: pathways and toxic effects of products, Journal of Environmental Science and Health,
 Part B 48 (2013) 927-934.
- 868 [61] B.A. Wols, D.J.H. Harmsen, E.F. Beerendonk, C.H.M. Hofman-Caris, Predicting
 869 pharmaceutical degradation by UV (LP)/H2O2 processes: A kinetic model, Chemical Engineering
 870 Journal 255 (2014) 334-343.
- [62] J.H. Baxendale, J.A. Wilson, The photolysis of hydrogen peroxide at high light intensities,
 Transactions of the Faraday Society 53 (1957) 344-356.
- [63] S. Giannakis, S. Rtimi, C. Pulgarin, Light-Assisted Advanced Oxidation Processes for the
 Elimination of Chemical and Microbiological Pollution of Wastewaters in Developed and
 Developing Countries, Molecules 22 (2017) 1070.
- 876 [64] T. Løgager, K. Sehested, J. Holcman, Rate constants of the equilibrium reactions $SO 4 + HNO3 \rightleftharpoons HSO 4 + NO.3$ and $SO 4 + NO 3 \rightleftharpoons SO 4 + NO.3$, Radiation Physics and Chemistry 41 (1993) 539-543.
- [65] M. Kwon, S. Kim, Y. Yoon, Y. Jung, T.-M. Hwang, J. Lee, J.-W. Kang, Comparative evaluation
 of ibuprofen removal by UV/H2O2 and UV/S2O82– processes for wastewater treatment,
 Chemical Engineering Journal 269 (2015) 379-390.
- [66] G.P. Anipsitakis, D.D. Dionysiou, Transition metal/UV-based advanced oxidation
 technologies for water decontamination, Applied Catalysis B: Environmental 54 (2004) 155-163.
 [67] Y. Xiao, L. Zhang, W. Zhang, K.-Y. Lim, R.D. Webster, T.-T. Lim, Comparative evaluation of
 iodoacids removal by UV/persulfate and UV/H2O2 processes, Water Research 102 (2016) 629639.
- [68] J. Deng, Y. Shao, N. Gao, S. Xia, C. Tan, S. Zhou, X. Hu, Degradation of the antiepileptic drug
 carbamazepine upon different UV-based advanced oxidation processes in water, Chemical
 Engineering Journal 222 (2013) 150-158.
- [69] O. Legrini, E. Oliveros, A.M. Braun, Photochemical processes for water treatment, Chemical
 Reviews 93 (1993) 671-698.
- [70] L. Zhou, M. Sleiman, C. Ferronato, J.-M. Chovelon, C. Richard, Reactivity of sulfate radicals
 with natural organic matters, Environmental Chemistry Letters 15 (2017) 733-737.
- [71] S. Miralles-Cuevas, D. Darowna, A. Wanag, S. Mozia, S. Malato, I. Oller, Comparison of
 UV/H2O2, UV/S2O82–, solar/Fe(II)/H2O2 and solar/Fe(II)/S2O82– at pilot plant scale for the
 elimination of micro-contaminants in natural water: An economic assessment, Chemical
 Engineering Journal 310 (2017) 514-524.
- [72] H.V. Lutze, S. Bircher, I. Rapp, N. Kerlin, R. Bakkour, M. Geisler, C. von Sonntag, T.C. Schmidt,
 Degradation of Chlorotriazine Pesticides by Sulfate Radicals and the Influence of Organic Matter,
 Environmental Science & Technology 49 (2015) 1673-1680.
- 901 [73] A. Adachi, T. Okano, Generation of Cyanide Ion by the Reaction of Hexamine and Losartan
 902 Potassium with Sodium Hypochlorite, Journal of Health Science 54 (2008) 581-583.
- 903 [74] M. Isidori, M. Bellotta, M. Cangiano, A. Parrella, Estrogenic activity of pharmaceuticals in
 904 the aquatic environment, Environment International 35 (2009) 826-829.
- 905 [75] H. Olvera-Vargas, N. Oturan, D. Buisson, E.D. van Hullebusch, M.A. Oturan, Electro-906 Oxidation of the Pharmaceutical Furosemide: Kinetics, Mechanism, and By-Products, CLEAN – 907 Soil, Air, Water 43 (2015) 1455-1463.
- 908 [76] N.S. Kudryasheva, T.V. Rozhko, Effect of low-dose ionizing radiation on luminous marine 909 bacteria: radiation hormesis and toxicity, Journal of Environmental Radioactivity 142 (2015) 68-910 77.
- 911 [77] V.L.K. Jennings, M.H. Rayner-Brandes, D.J. Bird, Assessing chemical toxicity with the 912 bioluminescent photobacterium (vibrio fischeri): a comparison of three commercial systems, 913 Water Research 35 (2001) 3448-3456.
- 914 [78] S. Rodriguez, A. Santos, A. Romero, Oxidation of priority and emerging pollutants with
- 915 persulfate activated by iron: Effect of iron valence and particle size, Chemical Engineering
- 916 Journal 318 (2017) 197-205.

- 917 [79] A.G. Trovó, T.F.S. Silva, O. Gomes, A.E.H. Machado, W.B. Neto, P.S. Muller, D. Daniel,
 918 Degradation of caffeine by photo-Fenton process: Optimization of treatment conditions using
 919 experimental design, Chemosphere 90 (2013) 170-175.
- 920 [80] E.P. da Costa, S.E.C. Bottrel, M.C.V.M. Starling, M.M.D. Leão, C.C. Amorim, Degradation of 921 carbendazim in water via photo-Fenton in Raceway Pond Reactor: assessment of acute toxicity
- 922 and transformation products, Environmental Science and Pollution Research (2018).
- [81] C. Tan, N. Gao, Y. Deng, Y. Zhang, M. Sui, J. Deng, S. Zhou, Degradation of antipyrine by UV,
 UV/H2O2 and UV/PS, Journal of Hazardous Materials 260 (2013) 1008-1016.
- [82] C. Richard, G. Guyot, A. Rivaton, O. Trubetskaya, O. Trubetskoj, L. Cavani, C. Ciavatta,
 Spectroscopic approach for elucidation of structural peculiarities of Andisol soil humic acid
 fractionated by SEC-PAGE setup, Geoderma 142 (2007) 210-216.
- [83] A. Paul, R. Stösser, A. Zehl, E. Zwirnmann, R.D. Vogt, C.E.W. Steinberg, Nature and
 Abundance of Organic Radicals in Natural Organic Matter: Effect of pH and Irradiation,
 Environmental Science & Technology 40 (2006) 5897-5903.
- [84] U. Kalsoom, S.S. Ashraf, M.A. Meetani, M.A. Rauf, H.N. Bhatti, Degradation and kinetics of
 H2O2 assisted photochemical oxidation of Remazol Turquoise Blue, Chemical Engineering
 Journal 200 (2012) 373-379.
- 934 [85] Y. Wang, F.A. Roddick, L. Fan, Direct and indirect photolysis of seven micropollutants in 935 secondary effluent from a wastewater lagoon, Chemosphere 185 (2017) 297-308.
- 936 [86] Y.-H. Guan, J. Ma, D.-K. Liu, Z.-f. Ou, W. Zhang, X.-L. Gong, Q. Fu, J.C. Crittenden, Insight into
- 937 chloride effect on the UV/peroxymonosulfate process, Chemical Engineering Journal 352 (2018)938 477-489.
- [87] R.G. Zepp, J. Hoigne, H. Bader, Nitrate-induced photooxidation of trace organic chemicals
 in water, Environmental Science & Technology 21 (1987) 443-450.
- 941 [88] G.-D. Fang, D.D. Dionysiou, Y. Wang, S.R. Al-Abed, D.-M. Zhou, Sulfate radical-based
- 942 degradation of polychlorinated biphenyls: Effects of chloride ion and reaction kinetics, Journal
 943 of Hazardous Materials 227-228 (2012) 394-401.
- [89] L. Patiny, A. Borel, ChemCalc: a building block for tomorrow's chemical infrastructure,Journal of Chemical Information and Modeling (2013).
- 946 [90] I. Dalmázio, L.S. Santos, R.P. Lopes, M.N. Eberlin, R. Augusti, Advanced Oxidation of Caffeine
- 947 in Water: On-Line and Real-Time Monitoring by Electrospray Ionization Mass Spectrometry,
- 948 Environmental Science & Technology 39 (2005) 5982-5988.

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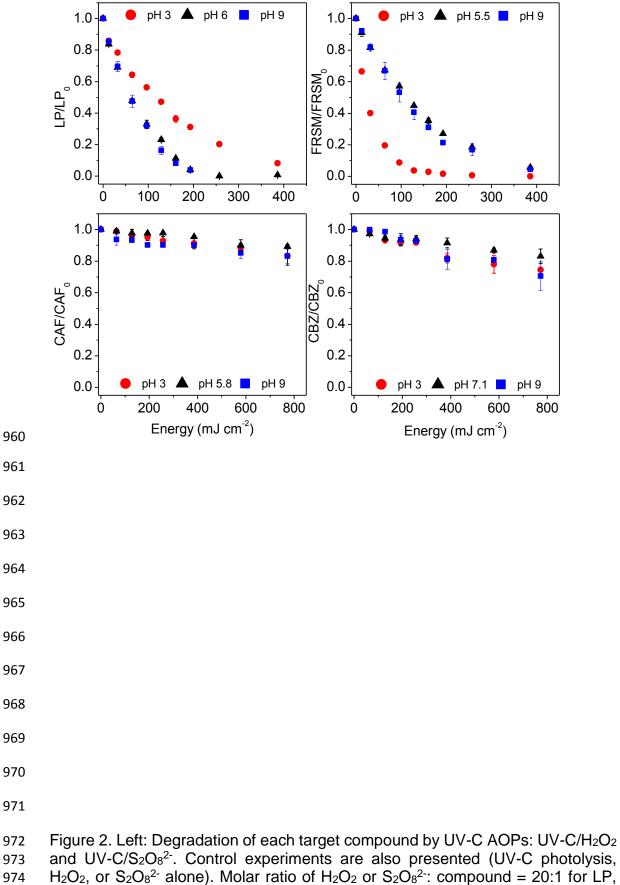
952 **GRAPHICAL ABSTRACT**



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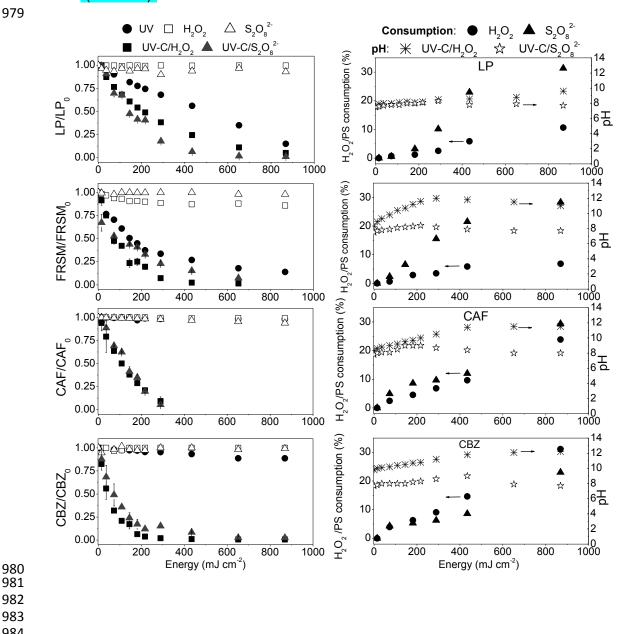
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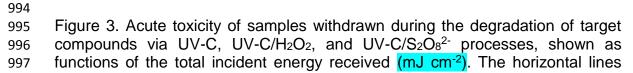
Figure 1. Photolysis (UV-C_{254nm}) of LP (2.2 μ M), FRSM (3.0 μ M), CAF (5.2 μ M), and CBZ (5.5 μ M) in ultrapure water at acidic, natural (non-adjusted), and basic pH ($I_0 = 2.54$ J m⁻² s⁻¹, volume 3.5 mL) as a function of incident energy per area (mJ cm⁻²).



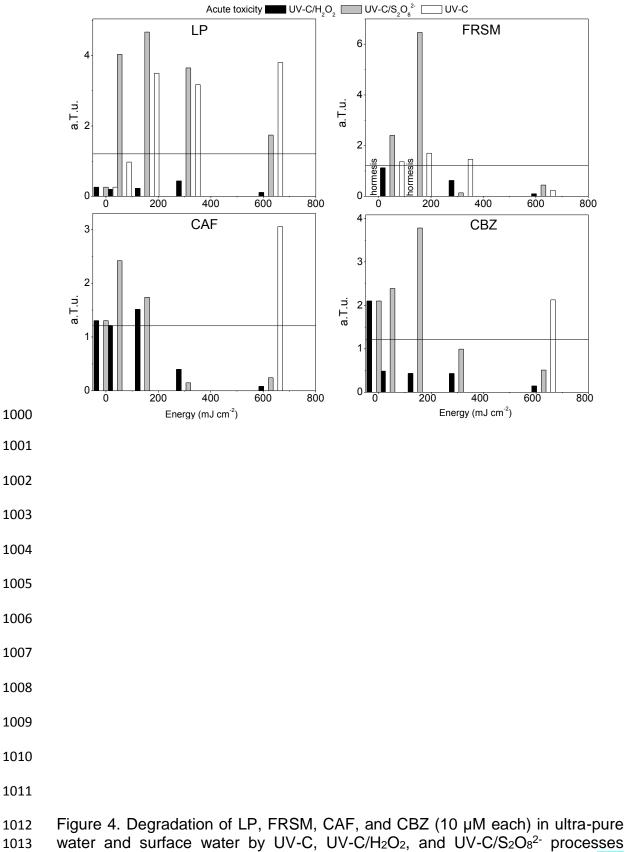
975 FRSM, and CAF, and 32:1 for CBZ; $I_0 = 2.41$ J m⁻² s⁻¹. Right: consumption (%) of

 H_2O_2 ($C_0 = 10^{-3}$ M), $S_2O_8^{2-}$ ($C_0 = 10^{-3}$ M), and pH values monitored during UV-C AOPs for each of the target compounds, as functions of incident energy per unit area (mJ cm⁻²).

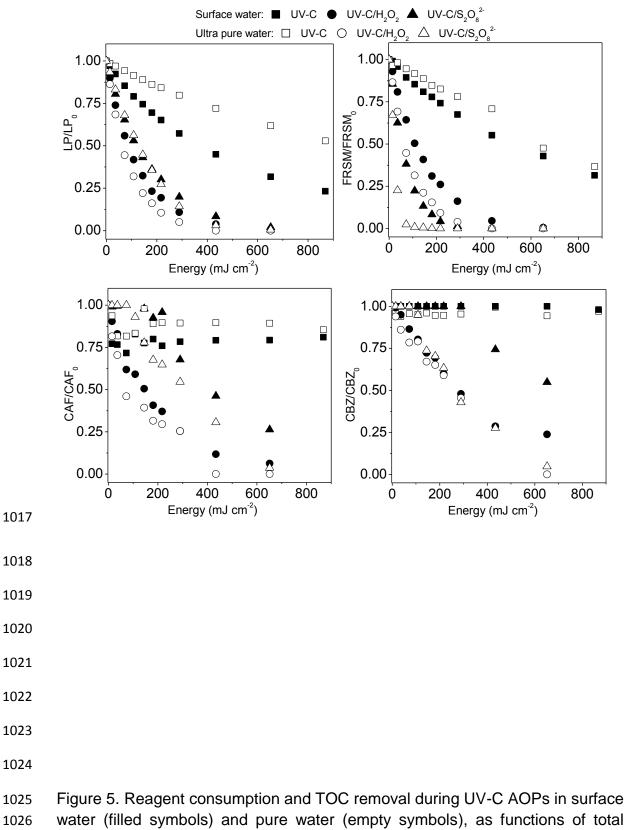




represent the threshold of 1.21 a.T.u.; bars crossing the line thus indicate toxic samples.



1014 ($C_{0\text{H}2O2 \text{ or } S2O82} = 10^{-3} \text{ M}$), shown as functions of total incident energy per area (mJ



water (filled symbols) and pure water (empty symbols), as functions of total incident energy per area (mJ cm⁻²) (Initial TOC in pure water 5.4 mg L⁻¹ and in surface water 6.6 mg L⁻¹).

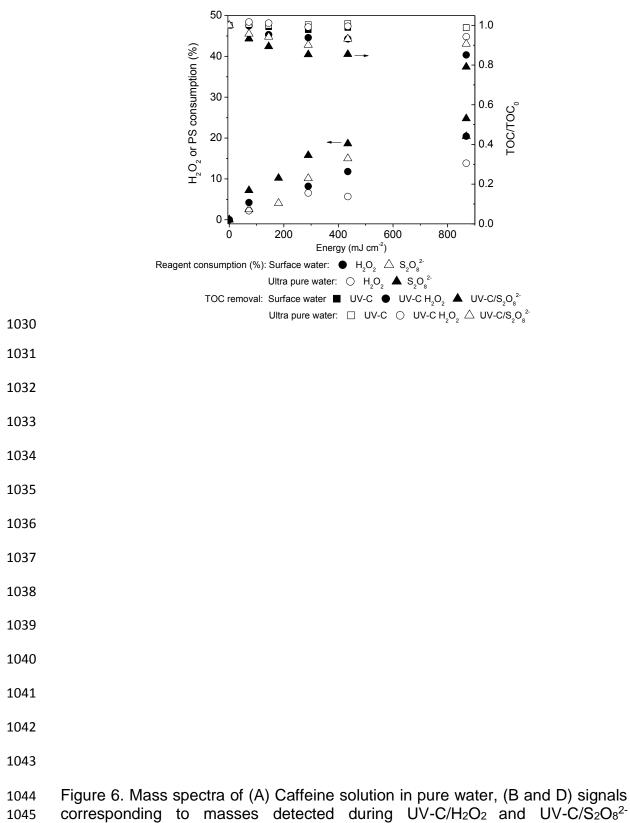


Figure 6. Mass spectra of (A) Caffeine solution in pure water, (B and D) signals corresponding to masses detected during UV-C/H₂O₂ and UV-C/S₂O₈²⁻ treatments, and (C and E) mass spectra obtained after UV-C/H₂O₂ and UV- $C/S_2O_8^{2-}$ treatments with 300 mJ cm⁻² of total incident energy.

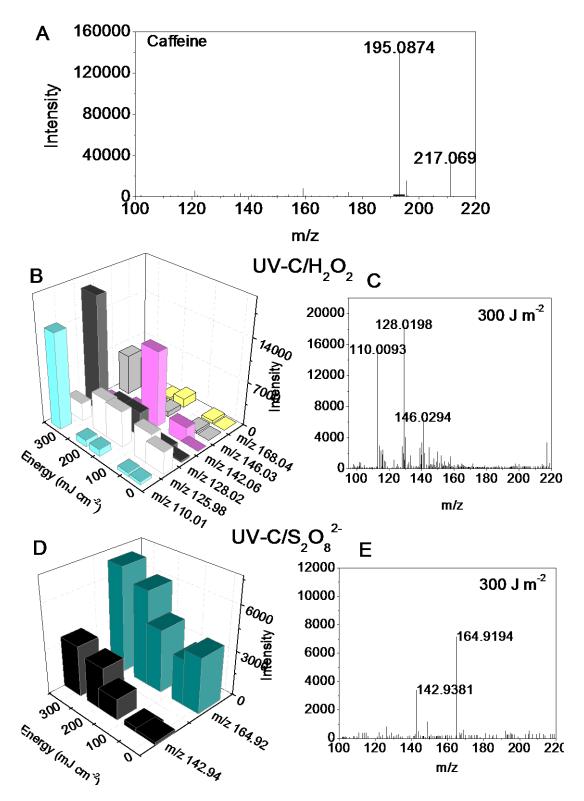


Figure 7. Degradation pathway proposed for the formation of transformation
 products generated during the oxidation of caffeine via UV-C/H₂O₂

